



# Polyester-derived monomers as microbial feedstocks: Navigating the landscape of polyester upcycling

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## ABSTRACT

Since their large-scale adoption in the early 20th century, plastics have become indispensable to modern life. However, inadequate disposal and recycling methods have led to severe environmental consequences. While traditional end-of-life plastics management had predominantly relied on landfilling, a paradigm shift towards recycling and valorization emerged in the 1970s, leading to the development of various, mostly mechano-chemical, recycling strategies, together with the more recent approach of biological depolymerization and upcycling. Plastic upcycling, which converts plastic waste into higher-value products, is gaining attention as a sustainable strategy to reduce environmental impact and reliance on virgin materials. Microbial plastic upcycling relies on efficient depolymerization methods to generate monomeric substrates, which are subsequently metabolized by native or engineered microbial systems yielding valuable bioproducts. This review focuses on the second phase of microbial polyester upcycling, examining the intracellular metabolic pathways that enable the assimilation and bioconversion of polyester-derived monomers into industrially relevant compounds. Both biodegradable and non-biodegradable polyesters with commercial significance are considered, with emphasis on pure monomeric feedstocks to elucidate intracellular carbon assimilation pathways. Understanding these metabolic processes provides a foundation for future metabolic engineering efforts, aiming to optimize microbial systems for efficient bioconversion of mixed plastic hydrolysates into valuable bioproducts.

## 1. Introduction

Since their inception in the early 20th century, plastics have become integral to daily life, with global production soaring from 1.5 Mt. in 1950 to 400 Mt. in 2023 (Statista, 2024). By 2020, the total mass of

plastics on Earth reached 8 Gt, twice that of all terrestrial and marine animals combined (Elhacham et al., 2020). This surge, coupled with inadequate disposal and/or recycling methods, has led to significant plastic waste accumulation, leading to greenhouse gas emissions, microplastic soil contamination, and overall severe land and sea

**Abbreviations:** 4HB, 4-hydroxybutyric acid; AA, adipic acid; ACP, acyl-carrier protein; ALE, adaptive laboratory evolution; Ara5P, D-arabinose 5-phosphate; BDO, 1,4-butanediol; BHAC,  $\beta$ -hydroxyaspartate cycle; BHET, bis(2-hydroxyethyl) terephthalate; BNC, bacterial nanocellulose; CA, Caproic acid; CDW, cell dry weight; CHMS, 4-carboxy-2-hydroxy-6-oxoheptanoate-6-semialdehyde; DAH, 1,6-diaminohexane; DAHP, 3-deoxy-D-arabino-heptulosonate 7-phosphate; DCD, 1,2-dihydroxy-3,5-cyclohexadiene-1,4-dicarboxylate; DHB, 2,4-dihydroxybutyric acid; DHBA, hydroxybenzaldehyde; DMAPP, dimethylallyl pyrophosphate; dTDP-L-rhamnose, deoxy-thymidine-diphospho-L-rhamnose; DXP, 1-deoxy-d-xylulose-5-phosphate; EG, ethylene glycol; FPP, farnesyl pyrophosphate; G3P, glyceraldehyde 3-P; GA, gallic acid; Gcl, glyoxylate carboxylase; Glu-1-P, glucose-1-phosphate; Glu-6-P, glucose-6-phosphate; GPP, geranyl diphosphate; HHA, 6-hydroxyhexanoic acid; HMBPP, 4-hydroxy-3-methyl-2-(E)-butenyl-4-diphosphate; IPP, isopentenyl pyrophosphate; LA, lactic acid; lcl-PHAs, long-chain-length PHAs; MA, muconic acid; mcl-PHAs, medium-chain-length PHAs; MEP, 2-C-methyl-D-erythritol-4-phosphate; MHET, mono(2-hydroxyethyl) terephthalate; MLA, malic acid; P3HB, poly(3-hydroxybutyrate); P4HB, poly(4-hydroxybutyrate); PBAT, Poly(butylene adipate-co-terephthalate); PBS, Polybutylene succinate; PBSA, Poly(butylene succinate-co-adipate); PCA, protocatechuic acid; PCL, polycaprolactone; PDC, 2-pyrone-4,6-dicarboxylic acid; PEP, phosphoenolpyruvate; PET, poly(ethylene terephthalate); PG, pyrogallol; PHAs, polyhydroxyalkanoates; PLA, poly(lactic acid); RPET, *R. jostii* strain PET; SA, succinic acid; scl-PHAs, short-chain-length PHAs; TaCo, tartonyl-CoA; TCA, tricarboxylic acid; TPA, terephthalic acid; UDP-Glu, uridine diphosphate glucose; VA, vanillic acid; WT, wild type; Xylu5P, D-xylulose 5-phosphate;  $\beta$ KA,  $\beta$ -ketoadipate.

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pollution (Pratiwi et al., 2024; Zhang et al., 2021). Substantial risks are posed to wildlife and ecosystems, from marine animals ingesting or becoming entangled in plastic debris (Morunga, 2024), to microplastics being found in various water bodies and food sources, eventually accumulating in cells and tissues (Al Mamun et al., 2023). Analyses on human liver and brain samples suggested an increasing trend of micro- and nanoplastics accumulation, with the total mass concentration of plastics in the brains having increased by about 50 % in the past 8 years (Nihart et al., 2025). Although the extent to which microplastics and nanoplastics could cause human harm and/or toxicity is yet unclear, several studies have established correlations between their presence and chronic biological effects and health hazards (Al Mamun et al., 2023).

### 1.1. Traditional end-of-life plastics management

Linear economy models for plastics that are based on a “take-make-dispose” approach, where fossil-based raw materials are extracted, transformed into products, and ultimately discarded as waste in landfills, are not sustainable due to both significant environmental deterioration and resource depletion. Conversely, the circular economy model focusing on “reduce-reuse-recycle-recover,” aims to create a sustainable system by designing long-lasting products while minimizing waste. End-of-life plastics management that has been solely focused on landfilling, started experiencing a paradigm shift in the early 1970s, when the first worldwide plastic waste recycling mill was established in Pennsylvania, USA (Lancan, 2023). Since then, four main types of plastics recycling processes have been developed, extensively studied, and optimized at industrial scale.

Primary recycling, also known as closed-loop recycling, involves reprocessing plastic waste into the same or similar products without significantly altering its chemical structure, while secondary recycling, or mechanical recycling, requires sorting, cleaning, shredding, and reprocessing plastics into pellets, flakes, or powders. These materials are then used to manufacture new plastic parts and products, often undergoing multiple cycles without significant performance loss (Schyns and Shaver, 2021). Although mechanical recycling is widely used for reprocessing plastic packaging, contributing significantly to Europe's average packaging recycling rate of 65 % in 2022 (European Commission Eurostat, 2025), it is severely constrained by material downcycling due to thermomechanical degradation from harsh remelting conditions.

Tertiary recycling, widely known as chemical recycling, has been extensively studied and widely adopted, as complete plastic depolymerization into oligomeric intermediates and/or their constituent monomeric feedstocks offers the potential for limitless recyclability (Liu et al., 2023). Pyrolysis, photocatalysis, and supercritical fluids are the main chemical methods for plastics processing. Pyrolysis, a well-established technique, uses heat to convert plastics into gases, liquid oils, and chars. Photocatalysis employs light and catalysts to break polymers into smaller molecules (Liu et al., 2023). Emerging approaches like solvolysis enable monomer recovery from polyesters at lower temperatures than pyrolysis, while supercritical fluids offer exceptional solubility and mass transfer properties for efficient plastic decomposition into gas, liquid, and solid product (Liu et al., 2023; Vollmer et al., 2020).

Mechanochemical plastic degradation is a form of chemical recycling that uses mechanical forces, such as grinding, milling, and shearing, to induce chemical transformations and recover valuable monomers or building blocks for material reuse (Zhou et al., 2023b). These processes lower the activation energy and increase the reaction rates by altering crystal structures and generating reactive species (Jicsinszky et al., 2023). Ultrasonication, the most common solution-phase method, creates elongational flow fields that stretch and break polymer chains, while ball milling induces transformations through collision and shear forces (Zhou et al., 2023b). Extrusion, a scalable and solvent-free process, applies heat and shear via rotating screws, leading to polymer softening, degradation, or crosslinking, depending on material

properties and processing conditions (Schyns and Shaver, 2021). While chemical and mechanochemical recycling hold promise as transformative plastic waste management solutions to counter plastic waste and resource depletion, process inefficiencies and high energy and cost requirements are still hindering their scalability (Pagola, 2023; Singh and Walker, 2024).

Quaternary recycling, more accurately referred to as waste-to-energy route, relies on incineration for the generation of heat and electricity. In several European countries, waste-to-energy incineration is part of district heating systems, offering renewable energy. Copenhagen's Amager Bakke facility, for instance, provides both electricity and district heating, supporting the city's carbon-neutral goals (State of Green, 2024). Sweden, often cited as a global leader in sustainability, has embraced waste-to-energy incineration to the extent that nearly half of its household waste is converted into energy, helping to keep landfill use at just 1 %, with 34 plants supplying heat and electricity to millions of homes (Welch et al., 2022). The carbon intensity of incineration is higher than renewable energy but lower than coal and, thus, its role in reducing carbon footprints depends on factors like waste composition and efficiency. As such, waste-to-energy should be part of a comprehensive strategy that includes waste reduction, recycling, and renewable energy adoption, rather than relied upon too heavily.

### 1.2. Biological plastics depolymerization

Biological depolymerization of plastics helps mitigate plastic waste accumulation by breaking down polymers into biodegradable components and offers an alternative to conventional mechanochemical recycling methods with low by-product generation. Microbial degradation involves the action of microorganisms such as bacteria and fungi, that break down polymers into simpler compounds or convert them into carbon dioxide, water, and new biomass, alongside the production of valuable biocompounds. In natural environments, this biodegradation process involves the secretion of extracellular enzymes that attach to the plastic surface, depolymerize it into oligomeric or monomeric compounds and, ultimately, allow microbial cells to assimilate them as carbon source. Enzyme-mediated biocatalytic depolymerization utilizes these specific enzymes to catalyze the breakdown of polymer chains in vitro, making the process highly selective and efficient (Mohanani et al., 2020).

The biodegradability of plastics is primarily determined by their chemical structure, with factors such as molecular composition, crystallinity, and the presence of hydrolysable bonds influencing the efficiency of biodegradation. Plastics with more chemically accessible and amorphous structures generally degrade more readily than those with highly crystalline or chemically resistant components. The efficiency of biodegradation is also highly dependent on specific environmental conditions. Although the latter might often be suboptimal in natural ecosystems, resulting in incomplete degradation (Wang et al., 2024b), proper waste management, such as industrial composting or controlled biodegradation, can ensure reintegration into biological cycles. All things considered, the incentivized growing demand for biodegradable plastics aligns with circular economy models, offering a more sustainable alternative to conventional plastics, which persist in the environment for centuries. This shift is reflected in market trends that highlight the increasing demand for sustainable and biodegradable materials across various industries. The global production volume of the non-biodegradable but widely used poly(ethylene terephthalate) (PET) was approximately 25 Mt. in 2023 but is projected to grow at a compound annual growth rate of only 4 % by 2030 (Statista, 2023). In contrast, the biodegradable poly(lactic acid) (PLA)—albeit only reaching 0.68 Mt. in 2023—is expected to grow significantly, with a compound annual growth rate exceeding 20 % between 2025 and 2030, according to a report published by Mordor Intelligence on the PLA market size and share analysis.

Biodegradation of plastics was first reported in the late 1960s, with a

mixed fungal culture degrading polyester polyurethane (Darby and Kaplan, 1968). The first pure microbial degrader, *Aureobasidium pullulans*, was identified in 1974 for its ability to degrade polycaprolactone (PCL), facilitated by PCL's hydrolysable ester bonds and low crystallinity (Fields et al., 1974). Subsequent studies in the 1970s and 1980s documented microbial degradation of PCL and polyvinyl alcohol by *Penicillium* and *Pseudomonas* species (Benedict et al., 1983; Shimao et al., 1983; Tokiwa and Suzuki, 1977). Research accelerated in the 1990s, with over 400 studies published by 2020, alongside a growing catalogue of plastic-degrading microorganisms and enzymes (Gambarini et al., 2022). Several databases, including PMBD (Gan and Zhang, 2019), PlasticDB (Gambarini et al., 2022), and PAZy (Buchholz et al., 2022), compile biodegradation data, with over 200 plastic-degrading enzymes and 800 microbial species being identified thus far (Gambarini et al., 2021). The field of enzyme-mediated plastic depolymerization is rapidly advancing, driven by innovations in protein engineering to enhance enzyme stability, specificity, and efficiency. Significant progress in rational design, directed evolution, and semi-rational approaches has led to notable improvements in enzymatic performance, while the integration of machine learning and artificial intelligence-based tools is further accelerating the discovery and optimization of plastic-degrading biocatalysts (Grigorakis et al., 2025).

### 1.3. Plastic waste upcycling

Plastic waste upcycling is the process of transforming plastic waste into new, higher-value products, that is rapidly gaining attention as an effective strategy to reduce environmental impact and decrease reliance on virgin materials. Microbial plastics upcycling heavily relies on efficient and chemically distinct depolymerization approaches to obtain plastic-derived monomers. The latter serve as carbon sources for microbial cultures that metabolize and transform them into valuable products. The first step, i.e., plastic depolymerization, can be achieved via different routes as outlined earlier, while the second step, i.e., production of added-value products, is based either on native or, more frequently, engineered microbial systems. Microbial metabolic engineering facilitates the development of modified microbial chassis capable of transforming plastic-derived monomers into industrially significant products. Undoubtedly, comprehensive approaches that integrate plastic degradation and the production of value-added compounds by a single system represent the ultimate goal for creating efficient and specialized microbial factories. These systems advance industrial biotechnology by upcycling waste materials into commercially valuable products while simultaneously reducing reliance on finite natural resources.

Polyesters are a class of plastics synthesized through polycondensation reactions between dicarboxylic acids and diols, characterized by the presence of ester functional groups in their main chain. Owing to their relatively labile chemical structure, polyesters are more readily depolymerized than other, more recalcitrant plastics. This inherent susceptibility to breakdown has made polyesters the primary focus of microbial upcycling research thus far, as they offer a more feasible route for bioconversion into value-added products.

This review focuses on the second phase of the microbial upcycling process of selected polyesters: the assimilation of polyester-derived monomers and their subsequent conversion into valuable bioproducts (Table 3). We selected both biodegradable and non-biodegradable polyesters that can be fully degraded into defined monomers and have commercial relevance, either with a significant market presence or projected growth. Most studies discussed here focus on pure monomeric feedstocks rather than mixed plastic hydrolysates—where literature remains limited—enabling precise elucidation of carbon assimilation pathways and demonstrating the upcycling potential of each microbial system. This knowledge lays the groundwork for the ultimate design of systems that efficiently convert mixed hydrolysates into valuable biocompounds. Our objective is to systematically identify and present the

intracellular metabolic pathways that have been demonstrated—or hypothesized—to be operable during microbial upcycling of their corresponding monomers. By elucidating these pathways, we aim to enhance the understanding of intracellular metabolism underlying the biosynthesis of value-added compounds, thereby providing a foundation for future metabolic engineering efforts to refine and optimize microbial upcycling strategies.

## 2. Selected polyesters and depolymerization monomers

Based on the criteria mentioned above, the biodegradable polyesters poly(butylene adipate-co-terephthalate) (PBAT), poly(butylene succinate) (PBS), poly(butylene succinate-co-butylene adipate) (PBSA), PCL, and PLA were included in the current discussion, along with the non-biodegradable PET (Fig. 1). Although PET is recyclable and amenable to controlled enzymatic degradation, it is not classified as biodegradable due to its high durability and resistance to natural degradation, as the process is inherently slow and environmentally insignificant.

### 2.1. Poly(ethylene terephthalate)

PET is a semi-aromatic, thermoplastic polyester synthesized through the polymerization of terephthalic acid (TPA) and ethylene glycol (EG). Known for its high mechanical strength, excellent barrier properties, and optical clarity, it is widely used in textiles and packaging. With over 55 Mt. produced globally in 2021, PET accounts for about 6 % of global polymer production, ranking among the “big five” polymers (Plastics Europe, 2023). Its physical properties vary based on processing, with crystallization degree significantly affecting its characteristics.

TPA (IUPAC: benzene-1,4-dicarboxylic acid) is an organic compound characterized by two carboxyl groups located at positions one and four of a benzene ring. TPA is a crucial precursor in the production of PET and serves as a fundamental building block for other polyesters, such as PBAT. Research has increasingly focused on the potential of TPA, derived from various polymers, for the synthesis of value-added compounds. Notably, several microorganisms have demonstrated the ability to assimilate TPA and produce a diverse array of valuable products. These include protocatechuic acid (PCA), various downstream aromatic and dicarboxylic acids,  $\beta$ -ketoadipate, lycopene, bacterial nanocellulose (BNC), and polyhydroxyalkanoates (PHAs) (Fig. 2, Table 1).

EG (IUPAC: ethane-1,2-diol) is a vicinal diol that emerges as the degradation product of the non-biodegradable polyester PET. Microbial assimilation of EG generates crucial intermediates like glycolate and glyoxylate, that can tap into the central carbon metabolism and enable the synthesis of various products, such as small aromatics, 2–4-dihydroxybutyric acid (DHB), BNC and PHAs (Fig. 3, Table 2).

### 2.2. Poly(lactic acid)

PLA is an aliphatic biodegradable polyester made from lactic acid (LA) units, with structural diversity based on the enantiomeric ratio. Poly(L-lactic acid) and poly(D-lactic acid) are semi-crystalline, while poly(D,L-lactic acid) is amorphous and degrades faster (de França et al., 2022). PLA's thermal, mechanical, optical, and barrier properties are comparable to PET, and it can be molded into various forms such as nanoparticles, films, and scaffolds. Initially limited to medical use due to high cost and low availability, advancements in production have expanded its applications to consumer goods, drug delivery, and tissue engineering (Khoury et al., 2024).

LA (IUPAC: 2-hydroxypropanoic acid) is a prominent chiral  $\alpha$ -hydroxy acid, that exists in two enantiomeric forms. The growing commercial interest in LA is largely due to its role as a precursor for PLA, although studies have demonstrated that it can also be converted into valuable bioproducts such as BNC, butyric and caproic fatty acids, and PHAs, highlighting its versatility and importance in sustainable bioprocesses (Fig. 3, Table 2).

**Table 3**

Summary of (engineered) upcycling microbial systems discussed in Chapter 3.

Added-value Product	Substrate	Microorganism	Outcome*	Reference
Protocatechuic acid	PET hydrolysate (3 mM TPA)	<i>E. coli</i> PCA-1	81 % MY after 3 h	(Kim et al., 2019)
	PET feedstock (65 mM)	<i>E. coli</i> M1B_M2F	0.9 % MYd after 120 h	(Zheng et al., 2024)
Gallic acid	TPA (3 mM)	GA-2b system ( <i>E. coli</i> PCA-1 & <i>E. coli</i> HBH-2)	93 % MY after 24 h	(Kim et al., 2019)
Catechol	TPA (3 mM)	<i>E. coli</i> CTL-1	90 % MY after 4 h	(Kim et al., 2019)
	TPA (3 mM)	<i>E. coli</i> MA-1	85 % MY after 6 h	(Kim et al., 2019)
Muconic acid	PET hydrolysate (32 mM TPA)	<i>P. putida</i> KT2440-tacRDL	68 % MY after 60 h	(Liu et al., 2022a, 2022b)
	PET hydrolysate (50 mM TPA & 50 mM EG)	TC-EM consortium (Pp-TC + Pp-EM)	33 % MY after 96 h (calculated on both)	(Bao et al., 2023)
	HHA (136 mM)	<i>E. coli</i> [pKK-AcChnDE]	86 % MYd after 82 h	(Y.-R. Oh et al., 2023)
Adipic acid	HHA from PCL (20 mM)	<i>E. coli</i> [pDSK-AcChnDE]	100 % MY after 16 h	(Y. R. Oh et al., 2022)
	TPA (1 mM)		79 % MY after 24 h	
	TPA from bottles (1 mM)	alg- <i>E. coli</i> pPCA1_pAA4	45 % MY after 24 h	(Valenzuela-Ortega et al., 2023)
Pyrogallol	TPA from hot stamping foils (1 mM)		66 % MY after 24 h	
	TPA (3 mM)	<i>E. coli</i> PG-1a strain	33 % MY after 6 h	(Kim et al., 2019)
Vanillic acid	TPA (3 mM)	VA-2a system ( <i>E. coli</i> PCA-1 & <i>E. coli</i> OMT-2 <sup>His</sup> )	42 % MY after 48 h	(Kim et al., 2019)
Vanillin	TPA (3 mM)	<i>E. coli</i> RAR-pVanX	74 % MY after 24 h	(Sadler and Wallace, 2021)
2-Pyrone-4,6-dicarboxylic acid	TPA (3 mM)	<i>E. coli</i> PCA & <i>E. coli</i> PDC <sub>TPA</sub>	99 % MY after 6 h	(M. J. Kang et al., 2020)
	BHET (124 mM)	<i>P. putida</i> AW165	76 % MY after 96 h	(Werner et al., 2021)
	PET hydrolysate (3 mM BHET)	<i>P. putida</i> AW165	45 % MY after 24 h	(Werner et al., 2021)
$\beta$ -Ketoadipic acid	TPA (3 mM)	<i>E. coli</i> $\beta$ KA	98 % MY after 72 h	(You et al., 2023)
	TPA (14 mM)			
	(two-stage bioconversion)	<i>E. coli</i> $\beta$ KA ( $\Delta$ poxB)	96 % MY after 24 h	(You et al., 2023)
Lycopene	mixed HDPE+PS + PET feedstock (350 mg)	<i>P. putida</i> AW307	24 % CY after 9 h	(Sullivan et al., 2022)
	TPA & EG (20 mM each)	<i>R. jostii</i> strain PET S6	0.004 % MY after 96 h (calculated on both)	(Diao et al., 2023)
	PET hydrolysate (429 mM TPA & 434 mM EG)	<i>R. jostii</i> strain PET S6	0.003 % MY after 60 h (calculated on both)	(Diao et al., 2023)
Polyhydroxyalkanoates	PET pyrolysate (20 mM TPA)	<i>P. putida</i> GO16	6 % MYd after 48 h	(Kenny et al., 2008)
	PET pyrolysate (20 mM TPA)	<i>P. putida</i> GO19	6 % MYd after 48 h	(Kenny et al., 2008)
	PET pyrolysate (20 mM TPA)	<i>P. frederiksborgensis</i> GO23	6 % MYd after 48 h	(Kenny et al., 2008)
	TPA (90 mM)	<i>P. putida</i> GO16	17 % MYd after 48 h	(Kenny et al., 2012)
	TPA (109 mM) & waste glycerol (201 mM)	<i>P. putida</i> GO16	16 % MYd after 48 h (calculated on both)	(Kenny et al., 2012)
	PET hydrolysate (30 mM TPA & 30 mM EG)	<i>P. umsongensis</i> GO16 KS3	1 % MYd after 28 h (calculated on both)	(Tiso et al., 2021)
	EG (100 mM)	<i>P. putida</i> MFL185	6 % MYd after 72 h	(Frandsen et al., 2018)
	AA (27 mM)	<i>P. putida</i> KT2440ge $\Delta$ PpaaF-paaYX::P14g $\Delta$ psrA	9 % CY after 48 h	(Ackermann et al., 2021)
	SA (42 mM)	<i>P. putida</i> mt-2	15 % CDW	(Shahid et al., 2013)
	SA (42 mM)	<i>R. palustris</i> SP5212	0.1 % MYd after 8 d	(Mukhopadhyay et al., 2005)
3-(3-hydroxyalkanoxyloxy) alkanolic acid	PET hydrolysate (50 mM TPA & 50 mM EG)	T-E consortium (Pp-T + Pp-E)	2 % MYd after 108 h (calculated on both)	(Bao et al., 2023)
	(fed-batch fermentation, one feeding)			
	TPA (17 mM)	<i>P. umsongensis</i> GO16 KS3 pSB01	1 % MYd after 28 h	(Tiso et al., 2021)
	TPA (60 mM)	<i>P. stutzeri</i> TPA3P	12 % CDW	(Liu et al., 2021)
	PET granules (2 M)	<i>I. sakaiensis</i> 201-F6	9 % CY after 6 d	(Fujiwara et al., 2021)
Poly(3-hydroxybutyrate)	SA (42 mM)	<i>C. glutamicum</i> DSM 20137	8 % CDW	(Shahid et al., 2013)
	SA (42 mM)	<i>B. megaterium</i> DSM 509	40 % CDW	(Shahid et al., 2013)
	LA (222 mM)	<i>R. eutropha</i> NRRL B14690	0.4 % MYd after 60 h	(Khanna and Srivastava, 2005)
Poly(4-hydroxybutyrate)	LA & acetic acid (pH-stat substrate titration; two-stage fed-batch culture)	<i>R. eutropha</i>	50 g/L	(Tsuge et al., 2001)
	BDO (60 mM)	<i>P. putida</i> NB10	8 % CDW	(Qian et al., 2023)
	BDO (80 mM) & octanoic acid (20 mM)	<i>P. putida</i> B10.2	5 % MY after 48 h	(Li et al., 2020)
Bacterial nanocellulose	TPA (120 mM)	<i>K. xylinus</i> DSM2004	4 % MYd after 18 d	(Esmail et al., 2022)
	TPA (120 mM)	<i>K. xylinus</i> DSM46604	0.8 % MYd after 18 d	(Esmail et al., 2022)
	TPA (n/a) & EG (47 mM)	<i>K. xylinus</i> DSM2004	0.6 g/L	(Esmail et al., 2022)
	TPA (n/a) & EG (7 mM)	<i>K. xylinus</i> DSM46604	0.2 g/L	(Esmail et al., 2022)
	EG (322 mM)	<i>K. xylinus</i> DSM2004	3.2 % MYd after 18 d	(Esmail et al., 2022)
	PLA hydrolysate (n/a)	<i>K. medellinensis</i> ID13488	4 g/L	(Sourkouni et al., 2023)
Glycolic acid	EG (0.5 M)	<i>Y. lipolytica</i> IMUFRJ 50682	86 % MY after 72 h	(Carniel et al., 2023)
	EG (2 mM)	<i>P. naganishii</i> AKU4267	88 % MY after 120 h	(Kataoka et al., 2001)
	EG (1 M)	<i>G. oxydans</i> DSM 2003	87 % MY after 48 h	(Wei et al., 2009)
	EG (2 mM)	<i>Rhodotorula</i> sp. 3Pr-126	92 % MY after 120 h	(Kataoka et al., 2001)
	EG (200 mM)	<i>Burkholderia</i> sp. EG13	99 % MY after 24 h	(Gao et al., 2014)
	EG (161 mM)	<i>E. coli</i> MG1655	80 % MYd after 140 h	(Pandit et al., 2021)

(continued on next page)



Table 3 (continued)

Added-value Product	Substrate	Microorganism	Outcome*	Reference
2,4-Dihydroxybutyric acid	EG from PET hydrolysate (11 mM)	<i>G. oxydans</i> KCCM 40109	99 % MY after 12 h	(Kim et al., 2019)
L-tyrosine	EG (45 mM)	<i>E. coli</i> TW354	2 % MY after 48 h	(Frazão et al., 2023)
Phenylalanine	EG (270 mM)	<i>E. coli</i> EGT01	6 % MY after 96 h	(Panda et al., 2023)
p-Coumaric acid	EG (160 mM)	<i>E. coli</i> EGP01	6 % MY after 96 h	(Panda et al., 2023)
Butyric acid	EG (160 mM)	<i>E. coli</i> EGC02	4 % MY after 96 h	(Panda et al., 2023)
Caproic acid	LA (32 mM)	<i>E. hallii</i> L2-7	70 % MY after 24 h	(Duncan et al., 2004)
	LA (29 mM)	<i>A. cacciae</i> L1-92	82 % MY after 24 h	(Duncan et al., 2004)
	LA (112 mM)	<i>M. hexanoica</i>	89 % MYd after 30 h	(S. Kang et al., 2022)
	LA (279 mM)	<i>R. bacterium</i> CPB6	33 % MYd after 6 d	(Zhu et al., 2017)
	LA (20 mM)	<i>M. elsdenii</i> J1	10 % MY after 40 h	(Marounek et al., 1989)
	BDO (20 mM)	<i>P. putida</i> KT2440	84 % MY after 49 h	(Li et al., 2020)
4-Hydroxybutyrate	BDO (111 mM)	<i>G. oxydans</i> DSM 50049	88 % MY after 24 h	(Ismail et al., 2024)
	PBAT hydrolysate (44 mM BDO & 9 mM AA)	<i>G. oxydans</i> DSM 50049	50 % MY after 10 h (calculated on BDO)	(Ismail et al., 2024)
Succinic acid	BDO (111 mM)	<i>G. oxydans</i> DSM 50049	50 % MY after 24 h	(Ismail et al., 2024)
Malic acid	BDO (444 mM)	<i>U. trichophora</i> AP037	33 % MYd after 15 d	(Phan et al., 2023)
Rhamnolipids	BDO (15 mM)	<i>P. putida</i> KT2440 B10.1 pPS05	9 % MYd after 4 d	(Utomo et al., 2020)
1,4-Butanediol	SA (n/a)	<i>E. coli</i> ECKh-422	n/a	(Yim et al., 2011)
1,6-Diaminohexane	AA (34 mM)	<i>E. coli</i> ΔsttA-DAH86	4 % MYd after 72 h	(Wang et al., 2023)

\* MY: molar yield, calculated as (mol of product / mol of substrate) x 100 %; MYd: mass yield, calculated as (g of product / g of substrate) x 100 %; CY: carbon yield, calculated as (mol of C in product / mol of C in substrate) x 100 %; CDW: cell dry weight; n/a: not available.

### 2.3. Poly( $\epsilon$ -caprolactone)

PCL is a synthetic, exclusively fossil-based polymer composed of 6-hydroxyhexanoic acid (HHA) units, chemically synthesized via the ring-opening polymerization of  $\epsilon$ -caprolactone (Suzuki et al., 2020). Known for its biocompatibility, biodegradability, and mechanical strength, PCL is often blended with hydrophilic or cationic polymers to form amphiphilic block copolymers used in drug delivery systems, such as nanocarriers for co-delivery of drugs and genes (Gaspar et al., 2016), as well as in biodegradable packaging (McLauchlin and Thomas, 2012). PCL's flexibility, low melting point, and blend compatibility make it highly processable for biomedical applications, including bone tissue engineering (Zaroog et al., 2019), catheters, blood bags, and implantable contraceptives (Mateos-Timoneda, 2009; Singh et al., 2021).

HHA (IUPAC: 6-hydroxyhexanoic acid) is a straight-chain omega-hydroxy fatty acid that is the only resulting monomer from the complete hydrolysis of PCL. Next to its repolymerization, it is also involved in the chemical production of adipic acid (AA), a precursor of nylon-6,6; AA production from HHA has also been microbially engineered (Fig. 2, Table 1).

### 2.4. Poly(butylene succinate)

PBS is a biodegradable, aliphatic thermoplastic polyester, synthesized from 1,4-butanediol (BDO) and succinic acid (SA) by condensation polymerization, and is of broad scientific and industrial interest due to its compostability according to ISO EN13432 standard (Barletta et al., 2022). PBS can be produced from both renewable and non-renewable monomers, though most commercial products are derived from fossil resources. It offers excellent melt processability, chemical resistance, and biodegradability, but its biodegradation is slow due to high crystallinity (Fredri and Dorigato, 2021). Due to its low Young's modulus, PBS is often blended with other polymers and additives to improve mechanical strength and expand its applications (Barletta et al., 2022). PBS is primarily used in food packaging, shopping bags, agriculture films, plant pots, and hygiene products, with limited use in biomedical applications due to insufficient biocompatibility (Fredri and Dorigato, 2021). The global PBS market is projected to grow at a compound annual growth rate of 20 % from 2022 to 2030, responding to the increasing demand from end-use industries (Grant View Research, 2025).

SA (IUPAC: butanedioic acid) is a dicarboxylic acid that can be derived from the degradation of PBS and PBSA, and, apart from its industrial applications, shows potential as a substrate for microbial upcycling. SA serves as a key intermediate in the tricarboxylic acid

(TCA) cycle and, as such, can serve as the carbon and energy source for the microbial production of valuable compounds, namely BDO and various types of PHAs (Fig. 3, Table 2).

BDO (IUPAC: butane-1,4-diol) is a primary alcohol and a key depolymerization monomer for PBS, PBSA, and PBAT. Numerous microorganisms, both native and engineered, can utilize BDO as a sole carbon source, either for biomass assimilation or towards the production of value-added products. The high-value products derived from the upcycling of BDO include 4-hydroxybutyric acid (4HB), poly(4-hydroxybutyrate) (P4HB), SA, malic acid (MLA), and rhamnolipids (Fig. 3, Table 2).

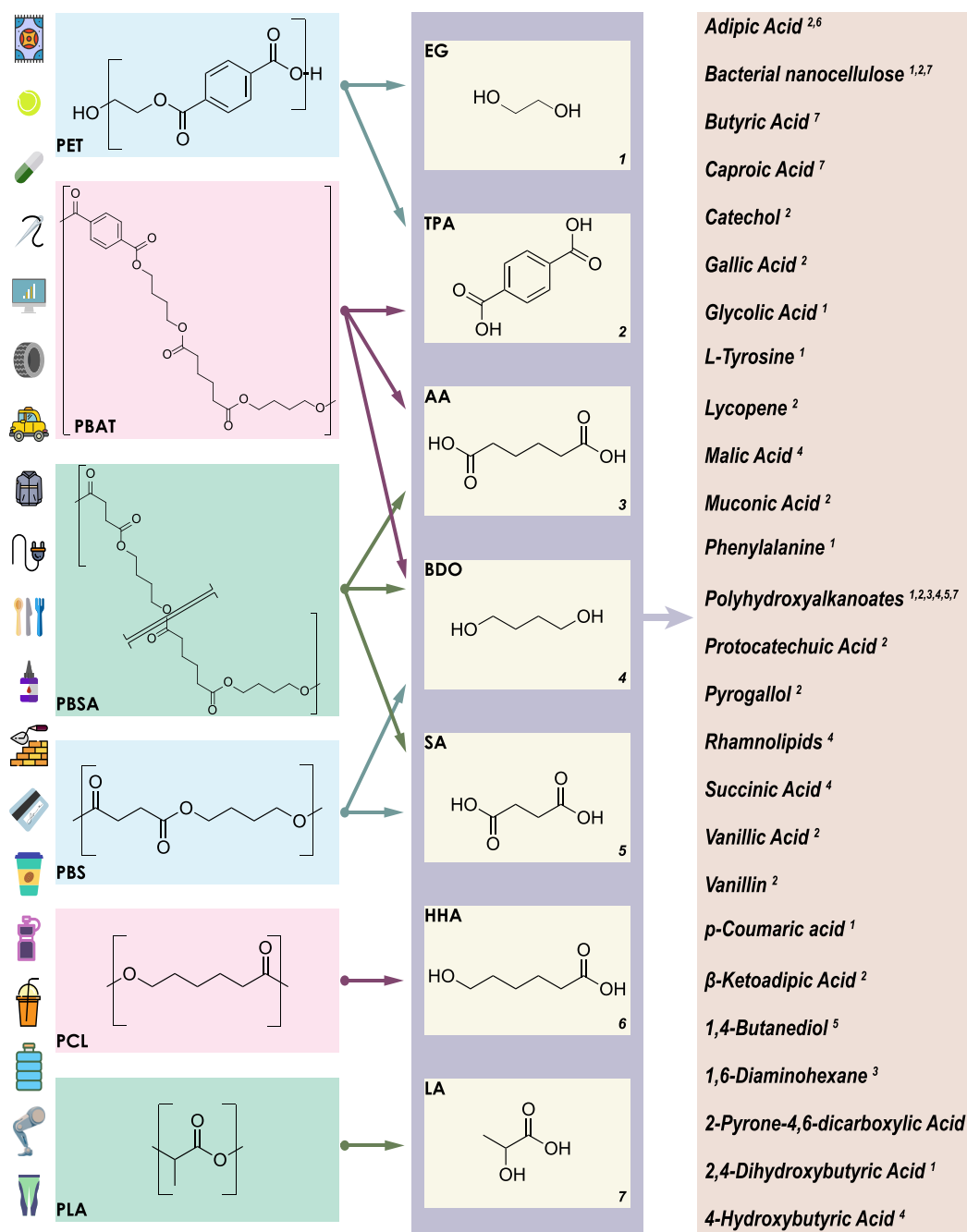
### 2.5. Poly(butylene succinate-co-butylene adipate)

PBSA is a biodegradable, fossil fuel-based aliphatic polyester synthesized from BDO, SA, and AA. It can be produced via polycondensation or transesterification of BDO with the dimethyl esters of SA and AA (Debuissy et al., 2017). This unique monomer combination gives PBSA excellent mechanical strength, flexibility, and thermal stability, making it suitable for various applications. While traditionally derived from fossil fuels, PBSA monomers can also come from bio-based feedstocks (Niaounakis, 2015). PBSA offers superior processability, lower melting temperature, lower crystallinity, and higher biodegradability than PBS (Debuissy et al., 2017). Its low crystallinity makes it ideal for film applications, particularly in the food industry, as well as in biomedical, life, and agricultural packaging (Aliotta et al., 2022; Wu, 2012).

AA (IUPAC: hexanedioic acid) is a dicarboxylic acid and one of the resulting monomers after hydrolysis of the heteropolymers PBAT and PBSA. Apart from its use for repolymerization, either for PBSA and PBAT (Debuissy et al., 2017; Jian et al., 2020), or for nylon-6,6 (Van Duuren et al., 2014), it can also be microbially upcycled to PHAs and 1,6-diaminohexane (DAH) (Fig. 2, Table 1).

### 2.6. Poly(butylene adipate-co-terephthalate)

PBAT is a biodegradable aromatic copolyester synthesized from BDO, AA, and TPA via random polycondensation. The inclusion of aliphatic components enhances its hydrolytic biodegradability, allowing it to degrade under composting conditions. With moderate crystallinity, good thermal stability, and strong processing stability, PBAT is ideal for extrusion and film blowing. It is promoted as a biodegradable alternative to low-density polyethylene, offering similar flexibility and resilience. PBAT is widely used in packaging and agricultural applications,



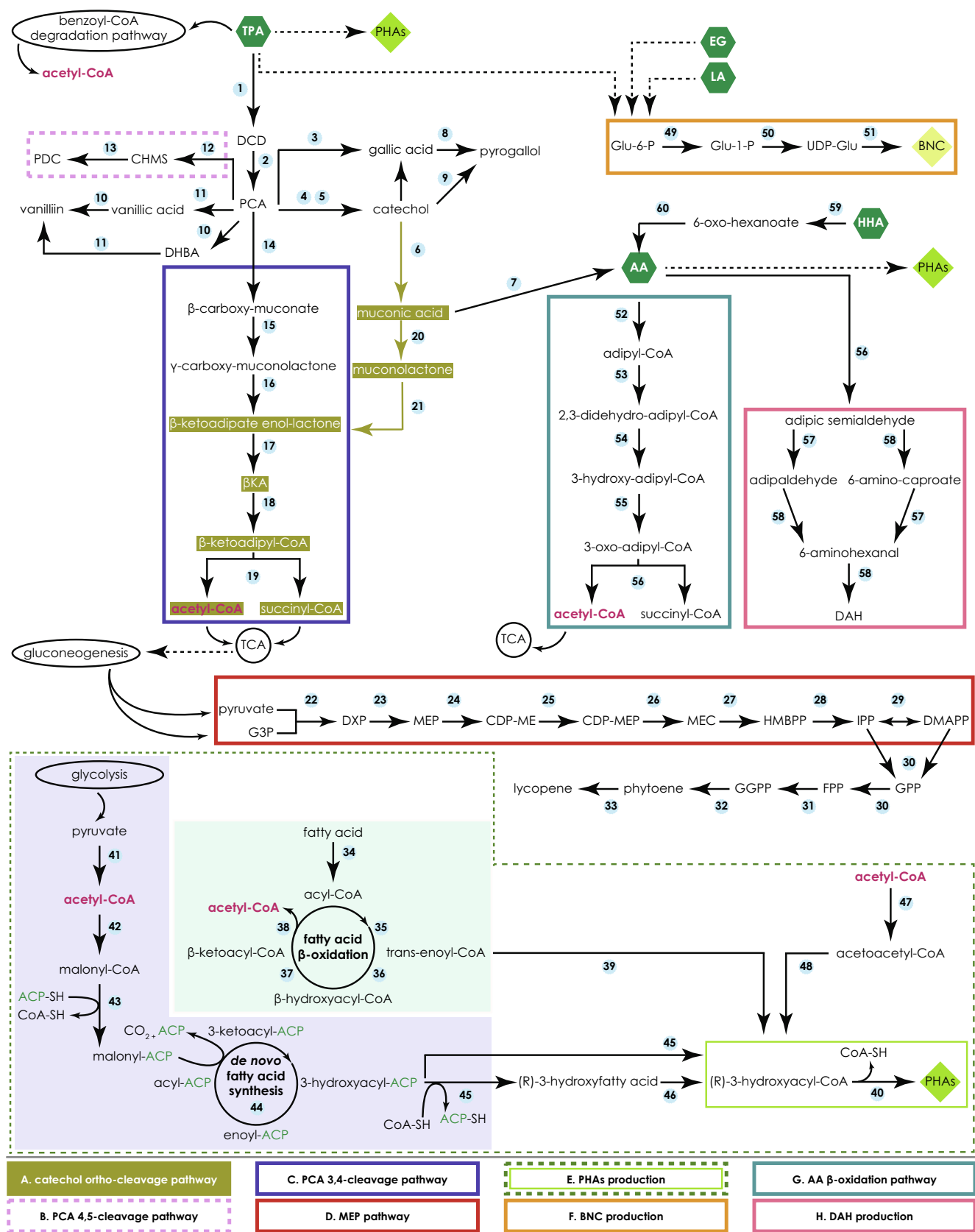
**Fig. 1. Chemical composition of polyesters, their corresponding monomers, and the monomer-derived added-value products of microbial upcycling.** The colored icons illustrate the commercial applications of polyesters. The superscript numbers in product names correspond to the monomers from where they were derived. The colored icons have been supplied as vector files and modified under a free license from the Vectreezy website (<https://www.vectreezy.com/>). PET, poly(ethylene terephthalate); PBAT, poly(butylene adipate terephthalate); PBSA, poly(butylene succinate-co-adipate); PBS, poly(butylene succinate); PCL, poly(ε-caprolactone); PLA, poly(lactic acid); EG, ethylene glycol; TPA, terephthalic acid; AA, adipic acid; BDO, 1,6-butanediol; SA, succinic acid; HHA, 6-hydroxycaproic acid; LA, lactic acid.

particularly for compostable bags and mulch films (Jian et al., 2020).

### 3. Microbial upcycling systems

Complete depolymerization of these polyesters yields seven distinct monomers, some of which are shared degradation products with broad biotechnological potential. Notably, multiple monomers can be converted into the same high-value compounds with diverse applications, from commodity and specialty chemicals to bioactive pharmaceuticals, food additives, and biopolymers (Section 4). TPA is extensively studied

for its role in producing short aromatic compounds, the carotenoid lycopene, BNC, and PHAs. EG can serve as a primary carbon source for anaerobic acetogenic bacteria, while it can also be assimilated aerobically via various natural and synthetic pathways. Currently, these have been coupled with the biosynthesis of glycolic acid, small aromatic compounds and PHAs. LA enters metabolism at the pyruvate level, supporting microbial production of BNC, PHAs, butyric acid, and caproic acid. BDO is a versatile substrate feeding into the TCA cycle, yielding MLA, SA, 4HB, P4HB, and rhamnolipids. AA can be microbially converted into PHAs and DAH, while HHA serves as a precursor for AA



(caption on next page)

**Fig. 2. Native and engineered intracellular metabolic pathways for assimilation and upcycling of polyester-derived monomers (part A).** Polyester-derived monomers are depicted in green hexagons. Dashed arrows indicate multistep processes. Numbers in grey octadecagons refer to enzymes catalyzing each reaction. Long and short names of enzymes can be found collectively in Table 1. AA, adipic acid; ACP, acyl carrier protein; CDP-ME, 4-diphosphocytidyl-2C-methyl-D-erythritol; CDP-MEP, 4-diphosphocytidyl-2C-methyl-D-erythritol-2-phosphate; CHMS, 4-carboxy-2-hydroxymuconate-6-semialdehyde; DAH, 1,6-diaminohexane; DCD, 1,2-dihydroxy-3,5-cyclohexadiene-1,4-dicarboxylate; DHBA, hydroxybenzaldehyde; DMAPP, dimethylallyl pyrophosphate; DXP, 1-deoxy-D-xylulose-5-phosphate; FPP, farnesyl pyrophosphate; G3P, glyceraldehyde 3-P; GGPP, geranylgeranyl diphosphate; GPP, geranyl diphosphate; HHA, 6-hydroxycaproic acid; HMBPP, 4-hydroxy-3-methyl-2-(E)-butenyl-4-diphosphate; IPP, isopentenyl pyrophosphate; MEC, 2C-methyl-D-erythritol-2,4-cyclodiphosphate; MEP, 2-C-methyl-D-erythritol-4-phosphate; BNC, bacterial nanocellulose; PCA, protocatechuic acid; PDC, 2-Pyrone-4,6-dicarboxylic acid; PHAs, polyhydroxyalkanoates; TCA, tricarboxylic acid cycle; TPA, terephthalic acid;  $\beta$ KA,  $\beta$ -ketoadipic acid. (For interpretation of the references to colour in this figure legend, the reader is referred to the web version of this article.)

biosynthesis.

### 3.1. PHAs biosynthesis

Evidently, numerous upcycling studies have focused on the production of PHAs, that constitute a diverse class of biodegradable and biocompatible polyesters and offer promising applications as sustainable bioplastics. PHAs accumulate as intracellular granules in microbial cells, primarily as energy reserves and in response to environmental stress, such as nutrient limitation or exposure to high temperatures, osmotic changes, and UV radiation. These granules serve a dual role, providing both a storage source and a protective mechanism for microbes under unbalanced growth conditions (Zhou et al., 2023a). The PHA diversity includes monomer structures, polymer chain structures, molecular weights, functionalization and all the combinations. To date, over 150 unique PHAs have been identified, which are generally categorized based on the carbon length of their monomeric units into short-chain-length PHAs (scl-PHAs; C<sub>3</sub>-C<sub>5</sub>), medium-chain-length PHAs (mcl-PHAs; C<sub>6</sub>-C<sub>14</sub>) and long-chain length PHAs (lcl-PHAs; >C<sub>15</sub>) (Ladhari et al., 2023). Scl-PHAs are known for their rigidity and strength, with polyhydroxybutyrates being among the most common species, while mcl-PHAs exhibit greater elasticity and flexibility, broadening the applicability of these biopolymers across various sectors (Pandey et al., 2022). Lcl-PHAs are less studied and much more rarely encountered, since only a few bacterial species have been shown to produce them, e. g., *Aureispira marina* and *Shewanella oneidensis* (Sehgal and Gupta, 2020).

PHAs can be synthesized as homopolymers, composed of a single type of monomer, or as copolymers, incorporating multiple different monomeric units. Mcl-PHAs are predominantly synthesized as copolymers and usually consist of C<sub>8</sub>-C<sub>12</sub> monomers, while scl-PHAs can be either homopolymers or copolymers, with the most common and the first industrially produced homopolymer being poly(3-hydroxybutyrate) (P3HB). This structural variability of PHAs allows for customization of physical and mechanical properties, enabling tailored applications (Zhou et al., 2023a). In the context of upcycling, PHAs represent a valuable microbial product from waste-derived carbon sources, providing a sustainable route to converting plastic waste into environmentally friendly materials with extensive commercial potential. Although the exact details of the molecular mechanisms governing microbial synthesis of PHAs, as well as the intricate interplay among different intracellular metabolic pathways, are not fully deciphered, it is established that this biosynthesis process has high energy demands, and can be separated into two stages, namely the generation of 3-hydroxyacyl-CoA and its subsequent polymerization into PHAs.

For the initial stage, microorganisms utilize three primary metabolic pathways, i.e., acetoacetyl-CoA synthesis, de novo fatty acid synthesis, and fatty acid  $\beta$ -oxidation (Fig. 2, Pathway E). All three pathways provide 3-hydroxyacyl precursors via different routes and then converge to the polymerization reaction catalyzed by PHA synthase (PhaC or PhbC), regardless of the length of the acyl group, to produce either homopolymers or copolymers (Mozejko-Ciesielska et al., 2019; Sathya et al., 2018).

Bacteria can produce PHAs from various carbon sources, including sugars and fatty acids, and adjust their metabolic pathways accordingly.

When using aliphatic carbon sources like fatty acids, bacteria utilize the  $\beta$ -oxidation pathway. In the  $\beta$ -oxidation cycle, fatty acids are first CoA-activated and then oxidized by acyl-CoA dehydrogenase to form trans-enoyl-CoA. Trans-enoyl-CoA is then hydrated by enoyl-CoA hydratase, producing (S)-3-hydroxyacyl-CoA, which undergoes a second oxidation step catalyzed by 3-hydroxyacyl-CoA dehydrogenase to yield 3-ketoacyl-CoA. In the final step of the cycle catalyzed by 3-ketoacyl-CoA thiolase, acetyl-CoA is released, and a shortened fatty acyl-CoA re-enters the cycle (Wang et al., 2024a). Notably, 3-ketoacyl-CoA thiolase and 3-hydroxyacyl-CoA dehydrogenase have been implicated in the monomer composition of produced PHAs (Mozejko-Ciesielska and Mostek, 2019; Ouyang et al., 2007). For PHA synthesis, a side reaction, facilitated by R- $\beta$ -hydroxyacyl-CoA hydratase (PhaJ), converts trans-enoyl-CoA to (R)-3-hydroxyacyl-CoA that is, subsequently, polymerized by PhaC.

For carbon sources unrelated to growth, the de novo fatty acid synthesis pathway is employed for PHA synthesis. Unlike the  $\beta$ -oxidation pathway, which degrades fatty acids to produce 3-hydroxyacyl-CoA intermediates, the de novo pathway synthesizes fatty acids directly, generating intermediates used to form monomers for PHA polymerization. In this pathway, carbon substrates are first converted to acetyl-CoA through glycolysis or other metabolic processes and then carboxylated to malonyl-CoA through the action of acetyl-CoA carboxylase. Fatty acid synthase, a multi-enzyme complex made of six enzymes and an acyl carrier protein, subsequently catalyzes successive cycles of condensation, reduction, dehydration, and a second reduction step, leading to the formation of long-chain acyl-carrier protein (ACP) fatty acid intermediates (Mashima et al., 2009). Among these intermediates, (S)-3-hydroxyacyl-ACP is either converted to the enantiomer (R)-3-hydroxyacyl-CoA by acyl-ACP:CoA transacylase (PhaG) (Hoffmann et al., 2000; Mozejko-Ciesielska et al., 2019), or first converted to (S)-3-hydroxy fatty acid by PhaG and then CoA-activated to (R)-3-hydroxyacyl-CoA by acyl-CoA synthase (alkK) (Chacón et al., 2024).

Another PHA biosynthesis pathway, initially identified and studied in *Zoogloea ramigera* and *Alcaligenes eutrophus* (Davis et al., 1987; Ploux et al., 1988; Schubert et al., 1988), begins with the condensation of two acetyl-CoA molecules, a reaction catalyzed by 3-ketothiolase (PhbA; PhaA). Acetoacetyl-CoA is then reduced to (R)-3-hydroxybutyryl-CoA by the enzyme acetoacetyl-CoA reductase (PhbB; PhaB). In the final step, the polymerization of (R)-3-hydroxybutyryl-CoA to P3HB is catalyzed by PHA synthase (PhbC; PhaC) through a condensation reaction. Although this pathway is usually used to produce P3HB, other scl-PHAs like P4HB can be synthesized via this route by forming the relevant intermediates (Sathya et al., 2018).

Based on the pathways described above, any microorganism capable of assimilating available carbon sources and converting them to acetyl-CoA can synthesize PHAs through any of these pathways, provided it possesses the genetic information for the necessary enzymatic machinery and the latter is operable under the given conditions.

### 3.2. Terephthalic acid

#### 3.2.1. PCA, downstream aromatics and dicarboxylic acids

The conversion of TPA to PCA is a key step of the TPA biodegradation pathway utilized by several aerobic bacterial species capable of



**Table 1**

Enzyme names as discussed in the text sections and presented in figure pathways with numerical codes corresponding to octadecagons in Fig. 2.

Section	Pathway	No	Long Name	Short Name(s)
3.2.1	Gallic acid production	1	TPA 1,2-dioxygenase	TPADO; TphAabc
		2	DCD dehydrogenase	DCDDH; TphB
		3	p-hydroxybenzoate hydroxylase	PobA
		4	PCA decarboxylase	AroY
		5	4-hydroxybenzoate decarboxylase	KpdB
	Catechol production	6	catechol dioxygenase	CatA
		7	enoate reductase	BcER
	Muconic acid production	8	pyrogallol decarboxylase	LpdC
		9	phenol hydroxylase	PhKLMNOPQ
		10	carboxylic acid reductase	CAR
		11	catechol O-methyltransferase	COMT
3.2.2	Pyrogallol production	12	PCA 4,5-dioxygenase	PCD4,5; LigAB
		13	CHMS dehydrogenase	LigC
		14	PCA 3,4-dioxygenase	PCD3,4; PcaHG
		15	3-carboxy-cis,cis-muconate cycloisomerase	PcaB
		16	4-carboxymuconolactone decarboxylase	PcaC
	Vanillic acid & vanillin production	17	β-ketoadipate enol-lactone hydrolase	PcaD; CatD
		18	β-ketoadipate succinyl CoA transferase	PcaIJ; CatIJ
	B. PCA 4,5-cleavage pathway	19	β-ketoadipyl CoA thiolase	PcaF; CatF
		20	muconate cycloisomerase	CatB
		21	muconolactone D isomerase	CatC
		22	DXP synthase	DXS
3.2.3	C. PCA 3,4-cleavage pathway	23	DXP reductoisomerase	DXR; IspC
		24	CDP-ME	IspD
		25	cytidyltransferase	IspE
		26	CDP-ME kinase	IspF
		27	MEC synthase	IspG
	D. MEP pathway	28	HMBPP synthase	IspH
		29	HMBPP reductase	IDI
	E. PHAs production	30	isopentenyl-diphosphate isomerase	IspA
		31	FPP synthase	CrtE
		32	GGPP synthase	CrtB
		33	phytoene synthase	CrtI
		34	phytoene desaturase	n/a
		35	thiokinase	n/a
		36	acyl-CoA dehydrogenase	n/a
		37	enoyl-CoA hydratase	n/a
		38	β-hydroxyacyl-CoA dehydrogenase	n/a
		39	β-ketoacyl-CoA thiolase	n/a
3.2.4	F. BNC production	40	R-β-hydroxyacyl-CoA hydratase	PhaJ
		41	PHA synthase	PhaC; PhbC
		42	pyruvate dehydrogenase	n/a
		43	acetyl-CoA carboxylase	ACC
		44	malonyl acetyl transacylase	n/a
	F. BNC production	45	fatty acid synthase	FASN
		46	acyl-ACP:CoA transacylase/ acyltransferase	phaG
		47	acyl-CoA synthase	alkK
		48	3-ketothiolase	PhbA; PhaA
		49	acetoacetyl-CoA reductase	PhbB; PhaB
		50	phosphoglucomutase	PGM
		51	UDP-Glu pyrophosphorylase	n/a
		52	cellulose synthase	Bcs

**Table 1 (continued)**

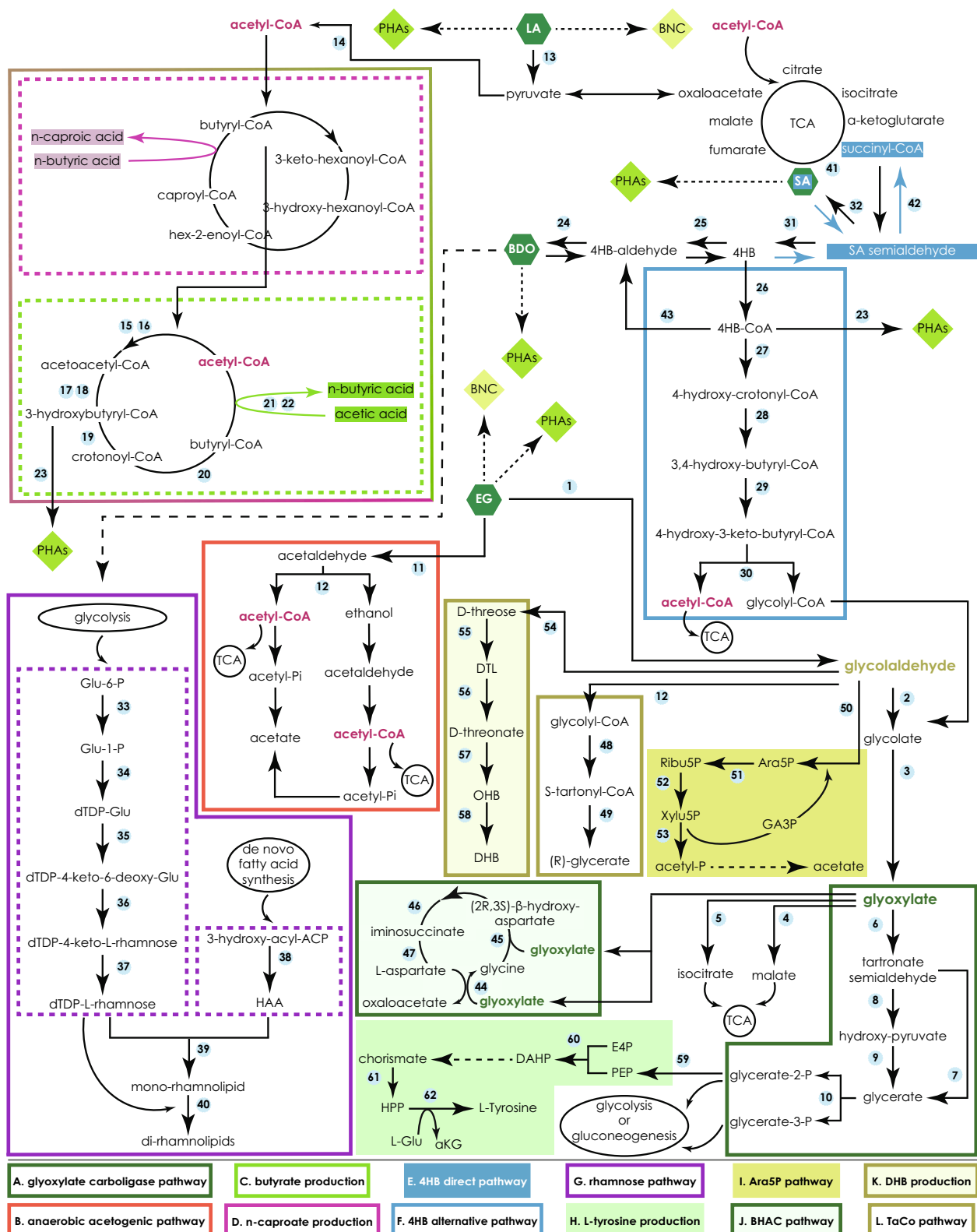
Section	Pathway	No	Long Name	Short Name(s)
3.7	G. Adipic acid β-oxidation pathway	52	CoA transferase	DcaIJ
		53	acyl-CoA dehydrogenase	DcaA
		54	enoyl-CoA hydratase	DcaE; PaaF; FaaB
		55	hydroxyacyl-CoA dehydrogenase	DcaH; PaaH
3.7.2	H. DAH production	56	acyl-CoA thiolase	DcaF; PaaJ; PcaF-1
		57	carboxylic acid reductase	CAR
3.8.1	Adipic acid production	58	transaminase	TA
		59	HAA dehydrogenase	ChnD
		60	6-oxohexanoate dehydrogenase	ChnE

n/a: not available.

metabolizing TPA as their sole carbon source, including *Comamonas* sp. E6, *Delftia tsyryhatensis* T7, and *Rhodococcus* sp. (Choi et al., 2005; Sasoh et al., 2006; Shigematsu et al., 2003). This pathway involves two critical enzymes, a TPA 1,2-dioxygenase (TPADO) which catalyzes the conversion of TPA to 1,2-dihydroxy-3,5-cyclohexadiene-1,4-dicarboxylate (DCD) and a DCD dehydrogenase, that further converts DCD to PCA (Fig. 2) (Salvador et al., 2019; Sasoh et al., 2006). The latter serves as a precursor for the subsequent production of various high-added value compounds and is also metabolized intracellularly via three distinct catabolic pathways: the 2,3-cleavage, the 3,4-cleavage, and the 4,5-cleavage pathway; all these funneling PCA to the TCA cycle (Nojiri et al., 2014). TPA could also be metabolized through anaerobic methanogenic processes, bypassing the PCA intermediate, with methane and/or carbon dioxide as end products (Kleerebezem and Lettinga, 2000). In this case, TPA catabolism proceeds via the benzoyl-CoA degradation pathway, as showcased in *Syntrophorhabdus aromaticivorans* UI, involving a series of sequential transformations leading to acetyl-CoA (Gao et al., 2022). However, neither anaerobic methanogens nor any microbial syntrophies of the oxic-anoxic interface with TPA-degrading potential have been the focus of any engineered studies towards plastic waste valorization, presumably due to the inherent difficulty of anaerobicity.

The biosynthetic route for PCA from TPA was engineered in *Escherichia coli* PCA-1 strain, incorporating the genes for the heterotrimeric O<sub>2</sub>-dependent TPA dioxygenase (TphAabc) and the NAD<sup>+</sup>-dependent DCD dehydrogenase (TphB) from *Comamonas* sp. E6. This engineered strain achieved conversion of TPA to PCA at a molar yield of 81 % within 3 h of incubation (Kim et al., 2019). Taking it a step further, an engineered *E. coli* strain was developed to combine both extracellular degradation of PET and intracellular conversion of TPA to PCA, allowing for efficient PET degradation and PCA production directly from PET feedstock. This was achieved by constructing a two-module biocatalytic system. Module 1 consisted of the membrane protein OmpA fused with a genetically optimized PETase (FAST-PETase: functional, active, stable and tolerant PETase) (Lu et al., 2022) to anchor the enzyme on the cell surface, facilitating both PET hydrolysis and intracellular incorporation of the resulting TPA. Module 2 involved the cytoplasmic pathway of TPADO and DCD dehydrogenase from *Comamonas* sp. E6. Optimization of enzyme expression, linker length between proteins, and reaction conditions achieved a maximum mass yield of about 1 % PCA after 120 h, illustrating the feasibility of PET upcycling despite the modest yield (Zheng et al., 2024).

**3.2.1.1. Gallic acid.** PCA can be converted to gallic acid (GA) by a PCA hydroxylase with meta-hydroxylation activity. An enzyme with this activity, p-hydroxybenzoate hydroxylase (PobA) from *Pseudomonas putida* KT2440, was expressed in *E. coli*, resulting in GA production from PCA with a molar yield of 40 % after 12 h. Further optimization was achieved by expressing a double-mutant version of the enzyme, PobA<sup>Mut</sup> (T294A/Y385F), in *E. coli* strain HBH-2, which led to an 84 % increase in



**Fig. 3. Native and engineered intracellular metabolic pathways for assimilation and upcycling of polyester-derived monomers (part B).** Polyester-derived monomers are depicted in green hexagons. Dashed arrows indicate multistep processes. Numbers in grey octagons refer to enzymes catalyzing each reaction. Long and short names of enzymes can be found collectively in Table 2. 4HB, 4-hydroxy-butyrate;  $\alpha$ KG,  $\alpha$ -ketoglutarate; ACP, acyl carrier protein; acetyl-P, acetyl phosphate; Ara5P, D-arabinose 5-phosphate; BDO, 1,4-butanediol; BHAC,  $\beta$ -hydroxyaspartate cycle; BNC, bacterial nanocellulose; DAHP, 3-deoxy-D-arabino-heptulosonate 7-phosphate; DHB, 2,4-dihydroxybutyric acid; dTDP-Glu, deoxythymidine diphosphate glucose; DTL, D-threono-1,4-lactone; EG, ethylene glycol; E4P, erythrose-4-phosphate; GA3P, glyceraldehyde 3-phosphate; Glu-1-P, glucose-1-phosphate; Glu-6-P, glucose-6-phosphate; HAA, 3-(3-hydroxy alkanoyl oxy) alkanonic acid; HPP, 4-hydroxyphenylpyruvate; LA, lactic acid; L-Glu, L-glutamate; OHB, 2-oxo-4-hydroxybutyrate; PEP, phosphoenolpyruvate; PHAs, polyhydroxyalkanoates; Ribul5P, D-ribulose 5-phosphate; SA, succinic acid; TaCo, tartronyl-CoA pathway; TCA, tricarboxylic acid; Xylul5P, D-xylulose 5-phosphate. (For interpretation of the references to colour in this figure legend, the reader is referred to the web version of this article.)

Table 2

Enzyme names as discussed in the text sections and presented in figure pathways with numerical codes corresponding to octadecagons in Fig. 3.

Section	Pathway	No	Long Name	Short Name(s)
3.3.1	Glycolate and glyoxylate production	1	PQQ quinone-dependent alcohol dehydrogenase	PedE; PedH
			1,2-propanediol oxidoreductase	FucO
			glycolaldehyde reductase	YqhD
			Zinc-dependent alcohol dehydrogenase	Gox0313
		2	glycolaldehyde dehydrogenase	PP_0545; PedI; AldA
			glycolate oxidase	GlcDEF
		3	malate synthase	GlcB
	A. Glyoxylate carboligase pathway	4	isocitrate lyase	AccA
		5	glyoxylate carboligase	Gcl
		6	tartronate semialdehyde reductase	GlxR
		7	hydroxypyruvate isomerase	Hyi
		8	hydroxypyruvate reductase	TtuD
		9	glycerate kinase	n/a
		10	aspartate-glyoxylate aminotransferase	BhcA
	J. $\beta$ -Hydroxyaspartate cycle	44	$\beta$ -hydroxyaspartate aldolase	BhcC
		45	$\beta$ -hydroxyaspartate dehydratase	BhcB
		46	iminosuccinate reductase	BhcD
		47	aldehyde dehydrogenase	PduP
	L. Tartronyl-CoA pathway	12	glycolyl-CoA carboxylase	
		48	tartronyl-CoA reductase	
		49	fructose 6-phosphate aldolase	FsaA
	I. D-arabinose 5-phosphate-dependent glycolaldehyde assimilation pathway	50	D-arabinose 5-phosphate isomerase	KdsD
		51	D-ribulose 5-phosphate 3-epimerase	Rpe
		52	phosphoketolase	CaPkt
		53	D-threose aldolase	Ec; FsaATA
		54	D-threose dehydrogenase	Pc.TadH
		55	D-threono-1,4-lactonase	Tt.Lac11
3.3.2	K. DHB production	56	D-threonate dehydratase	Hh.AraD
		57	2-oxo-4-hydroxybutyrate reductase	Ec; Mdh5Q
		58	Enolase	Eno
		59	DAHP synthase	AroG
		60	chorismate mutase/prephenate dehydrogenase	TyrA
	H. L-tyrosine production	61	transaminase	
		62	propane diol dehydratase	PduCDE
		11	CoA-dependent propionaldehyde dehydrogenase	PduP
		12	lactate dehydrogenase	LDH
		13	pyruvate dehydrogenase	PDH
3.3.3	PHAs	14	acetyl-CoA acetyltransferase	AtoB
		15		
		16		
3.3.4	B. Anaerobic acetogenic pathway	16	3-ketothiolase	PhbA; PhaA
		17	3-hydroxybutate dehydrogenase	Hbd

Table 2 (continued)

Section	Pathway	No	Long Name	Short Name(s)
3.5.1	F. 4HB alternative oxidation pathway	18	acetoacetyl-CoA reductase	PhbB; PhaB
		19	enoyl-CoA hydratase	Crt
		20	butyryl-CoA dehydrogenase	Bcd
		21	butyryl-CoA:(acceptor) oxidoreductase	But; CoAT
		22	butyrate kinase	buk
		23	PHA synthase	PhbC; PhaC
		24	aldehyde dehydrogenase	ADH; adhE2
		25	alcohol dehydrogenase	ADH
		26	4HB-CoA transferase	Cat2
		27	acyl-CoA dehydrogenase	n/a
	E. 4HB direct oxidation pathway	28	enoyl-CoA hydratase	n/a
		29	3-hydroxyacyl-CoA dehydrogenase	n/a
		30	acetyl-CoA acetyltransferase	n/a
		31	4HB dehydrogenase	4HBd
		32	succinate semialdehyde dehydrogenase	n/a
		33	phosphoglucomutase	PGM
		34	G1P thymidyltransferase	RmlA
3.5.3	G. Rhamnose pathway	35	dTDP-D-glucose 4,6-dehydratase	RmlB
		36	dTDP-6-deoxy-D-xylo-4-hexulose 3,5-epimerase	RmlC
		37	dTDP-6-deoxy-L-lyxo-4-hexulose reductase	RmlD
		38	3-hydroxyacyl-ACP-O -3 hydroxyacyltransferase	RhlA
		39	rhamnosyltransferase I	RhlB
		40	rhamnosyltransferase II	RhlC
		41	succinyl-CoA synthetase	SucCD
		42	CoA-dependent succinate semialdehyde dehydrogenase	SucD
		43	4HB-CoA reductase	n/a

n/a: not available; PQQ: pyrroloquinoline quinone; dTDP: deoxythymidine diphosphate.

GA production compared to the wild type (WT) PobA. For GA production directly from TPA, the strains PCA-1 and HBH-2 were co-cultured to facilitate the sequential conversion of TPA to PCA and, subsequently, PCA to GA. Under the optimized co-culturing conditions, the GA-2b system achieved a molar yield of 93 % for the conversion of TPA to GA after 24 h, without the accumulation of PCA (Kim et al., 2019).

3.2.1.2. *Catechol*. Catechol is another valuable aromatic compound that can be produced from PCA via decarboxylation. This conversion was demonstrated using the enzyme AroY, a highly conserved PCA decarboxylase, expressed in *E. coli* strain CTL-1, which achieved a 98 % molar yield of catechol from PCA after 5 h. Strain CTL-1, co-expressing TphAabc, TphB, and AroY, converted TPA to catechol with a molar yield of 90 % without PCA accumulation after 4 h (Kim et al., 2019).

3.2.1.3. *Muconic acid*. Catechol can serve as a precursor for the biosynthesis of muconic acid (MA) through ring cleavage (Fig. 2, Pathway A). This conversion was successfully achieved by *E. coli* strain CDO-1 via expression of CatA—a non-heme Fe(III)-dependent catechol 1,2-dioxygenase from *P. putida* KT2440. To establish the biosynthetic pathway for MA production starting from TPA, the MA biosynthesis pathway was combined with the catechol biosynthetic route of *E. coli* strain CTL-1. The resulting engineered strain, i.e., MA-1, effectively converted TPA to MA with a molar yield of 85 % after 6 h of incubation,

without the accumulation of intermediate compounds (Kim et al., 2019). Another study focused on valorization of PET hydrolysates towards MA production via engineering *P. putida* KT2440; the inherent conversion of PCA to MA via catechol by this strain had already been established (Johnson et al., 2016). The strain was modified to integrate both a TPA degradation pathway and a pathway for MA production via its intermediates. To serve the first purpose, genes encoding a proto-catechuate 3,4-dioxygenase (*pcaHG*) were replaced by the *tph* cluster from *Pseudomonas stutzeri*, which included a transcriptional regulator (TphR), a TPA transporter (TpaK), the TphAabc TPADO, and the TphB DCD dehydrogenase. Additionally, codon-optimized genes for a proto-catechuate decarboxylase (*aroY*) and a flavin prenyltransferase (*ecdB*) from *Enterobacter cloacae* were introduced to enhance catechol production. Overexpression of CatA, together with deletions of the downstream metabolic genes i.e., muconate lactonase (*catB*) and muconolactone isomerase (*catC*), were performed to set up the MA biosynthetic pathway. The resulting engineered strain, *P. putida* KT2440-tacRDL, achieved efficient conversion of TPA to MA with a molar yield of 100 % under optimized conditions. This multifunctional strain successfully produced 0.5 g MA/g PET, reaching 68 % of the theoretical conversion rate, demonstrating its potential for sustainable PET upcycling (Liu et al., 2022b).

**3.2.1.4. Adipic acid.** AA is another commercially important platform chemical that can be produced via the PCA branch, through a shortcut of the catechol ortho-cleavage catabolic pathway. Eight genes, essential for the complete conversion of TPA down to AA, were engineered in *E. coli*, organized in two separate vectors (Valenzuela-Ortega et al., 2023). TPA conversion to PCA was achieved by the *Comamonas* sp. E6 TphA<sub>abc</sub> and TphB enzymes, while PCA conversion to AA involved the sequential action of the PCA decarboxylase AroY from *Klebsiella pneumoniae*, a subunit of the 4-hydroxybenzoate decarboxylase KpdB from *K. pneumoniae*, responsible for AroY activation by generation of prenylated flavin mononucleotide, the CatA catechol dioxygenase from *P. putida*, and finally the [4Fe–4S]-dependent enoate reductase BcER from *Bacillus coagulans* (Joo et al., 2017), responsible for muconic acid reduction to AA. When grown on TPA, the double-vector transformed *E. coli* strain could not perform MA hydrogenation to AA, therefore, only reaching MA production, albeit at a yield of 92 %. The use of polycistronic mRNA for tighter translation control and alginate hydrogels for cell immobilization, led to the alg-*E. coli* pPCA1<sub>-pAA4</sub> strain that produced AA with a yield of 79 %, corresponding to 115 mg/L. As proof of concept, the valorization of post-consumer PET bottles and hot stamping foils was investigated, via alkaline depolymerization of PET and subsequent conversion of the resulting TPA to AA by the above-mentioned *E. coli* engineered strain. These processes yielded 65 mg/L and 96 mg/L AA (66 % yield), from PET bottles and hot stamping foils, respectively (Valenzuela-Ortega et al., 2023).

**3.2.1.5. Pyrogallol.** Pyrogallol (PG) can also be biosynthesized via the PCA branch, either through decarboxylation of GA derived from PCA hydroxylation, or hydroxylation of catechol produced via PCA decarboxylation. To achieve PG synthesis via GA, the GA decarboxylase LpdC from *Lactobacillus plantarum* (Jiménez et al., 2013) was integrated into the engineered *E. coli* strain HBH-2 capable of GA biosynthesis, resulting in the construction of *E. coli* strain PG-1a, expressing TphAabc, TphB, Poba<sup>Mut</sup>, and LpdC. This strain produced PG from TPA at a molar yield of 33 % after 6 h; however, it also generated catechol as a byproduct due to the promiscuous activity of LpdC towards PCA. To address catechol accumulation, a secondary pathway was developed that utilized the *PhKLMNOPQ* operon from *P. stutzeri* OX1 coding for the complete protein machinery of a phenol hydroxylase that has been shown to promiscuously hydroxylate catechol to PG (Wang et al., 2018). The engineered *E. coli* strain CH-1 expressing a functional PH converted catechol to PG with a yield of 67 %, although when combined with the

original GA biosynthesis pathway from strain PG-1b, the accumulation of catechol persisted, and PG production was lower than in PG-1a. An alternative strategy for PG biosynthesis was constructed by integrating PCA conversion to catechol using AroY, followed by catechol hydroxylation to PG using the enzymatic machinery produced by *phKLMNOPQ* from *P. stutzeri* OX1. The optimized PG-2b system, combining *E. coli* strains CTL-1 and CH-1 in a co-culture, achieved a molar yield of 19 % for PG production, although a substantial amount of catechol remained unconverted (Kim et al., 2019).

**3.2.1.6. Vanillic acid.** PCA can also be converted to vanillic acid (VA) by the action of a catechol O-methyltransferase (COMT) when S-adenosyl methionine serves as a co-substrate. Various OMTs were heterologously expressed in *E. coli* BL21 and, among them, OMT from *Homo sapiens* (HsCOMT) demonstrated the highest molar yield of VA from PCA at 29 % (Kim et al., 2019). To facilitate production of VA from TPA, a biosynthetic pathway comprising TphAabc and TphB for PCA production, along with HsOMT, was constructed in the engineered strain *E. coli* VA-1. Nonetheless, complete consumption of 3 mM TPA within 72 h yielded just 0.6 % VA, while accumulation of PCA was observed. To enhance the low conversion rate of PCA to VA, the modified strain OMT-2<sup>His</sup> was developed, where a hexameric histidine was attached to the N-terminus of HsOMT for increased protein solubility. *E. coli* OMT-2<sup>His</sup> growth in a medium supplemented with methionine in equimolar concentrations to PCA, resulted in an increased molar yield of VA up to 45 %. Further improvement of PCA conversion to VA was achieved using a double-catalyst system, VA-2a, with the strains PCA-1 and OMT-2<sup>His</sup> added in the co-culture at a 1:3 cell density ratio. The VA produced from TPA increased to a yield of 9 % after 48 h, although the molar yield from PCA remained at 6 %. Enhancing oxygen supply through improved aeration in the VA-2b system increased ATP generation, raising the molar yield of VA from TPA by 4.7-fold, albeit with about 40 % of TPA remaining unconverted. Optimizing the initial cell ratio of the two strains, as well as the fluxes of TPA to PCA and PCA to VA, was deemed essential for further improvement of the overall conversion efficiency (Kim et al., 2019).

**3.2.1.7. Vanillin.** Vanillin is another aromatic compound that can be produced via the PCA branch, through two similar enzymatic pathways guided by the action of a carboxylic acid reductase (CAR) and a COMT. CAR can catalyze both the reduction of PCA to hydroxybenzaldehyde (DHBA) and the conversion of VA to vanillin, while COMT catalyzes both PCA or DHBA methylation to VA and vanillin, respectively. *E. coli* MG1655 RARE strain, known for its reduced aromatic aldehyde reduction properties, was engineered to convert TPA all the way to vanillin (Sadler and Wallace, 2021). The necessary enzymes were assembled into two vectors: pVan1, coding for the TPA 1,2-dioxygenase and the DCD dehydrogenase from *Comamonas* sp. E6, and pVan2, coding for a *Nocardia iowensis* carboxylic acid reductase (NiCAR), and a point mutant of the soluble form of catechol O-methyltransferase (S-COMT Y200L) from *Rattus norvegicus*. Additionally, a third plasmid, pSfp, encoding a phosphopantetheinyl transferase from *Bacillus subtilis*, was introduced to facilitate post-translational modification of NiCAR. The resulting strain, *E. coli* RARE-pVanX, produced detectable amounts of vanillin from TPA, although the conversion was initially less than 1 %, with significant accumulation of the intermediates PCA, DHBA and VA. Following optimization of culture conditions, including pH, temperature, incubation time, and the addition of L-methionine, n-butanol, and oleyl alcohol to improve membrane permeability and in situ product removal, the biotransformation was significantly improved, resulting in a maximum molar yield of 74 %. The engineered pathway was further employed to demonstrate the upcycling potential of post-consumer PET waste into vanillin, by coupling enzymatic PET hydrolysis by the thermostable LCC<sup>WCCG</sup> (Tournier et al., 2020) with vanillin production from the released TPA by *E. coli* RARE\_pVanX (Sadler and Wallace, 2021).



### 3.2.2. PCA 4,5-cleavage pathway

In the PCA 4,5-cleavage pathway (Fig. 2, Pathway B), PCA is transformed into 4-carboxy-2-hydroxymuconate-6-semialdehyde (CHMS) by PCA 4,5-dioxygenase (PCD<sub>4,5</sub> and LigAB). CHMS is then non-enzymatically converted to an intramolecular hemiacetal form and, eventually, oxidized to 2-pyrone-4,6-dicarboxylic acid (PDC) by CHMS dehydrogenase (LigC) (Harwood and Parales, 1996). To enable TPA conversion to PDC, *E. coli* XL1-Blue strain was transformed with two separate vectors, encoding the necessary genes for TPA conversion to PCA (TphA<sub>abc</sub> and TphB) and PCA conversion to PDC (ligAB and ligC), respectively (Kang et al., 2020). The resulting engineered *E. coli* PDC<sub>TPA</sub> achieved a molar yield of 91 % PDC from TPA. To further optimize this process, a double-catalyst system was developed by combining *E. coli* PCA strain for TPA degradation and *E. coli* PDC<sub>PCA</sub> strain for PDC synthesis, in a co-culture with a 3:5 cell density ratio. The system achieved a 99 % molar yield conversion of TPA to PDC, without accumulating PCA after 6 h of incubation.

### 3.2.3. PCA 3,4-cleavage pathway

During the PCA 3,4-cleavage pathway (Fig. 2, Pathway C), also known as ortho-cleavage or  $\beta$ -ketoadipate ( $\beta$ KA) pathway, PCA is converted to 3-carboxy-*cis,cis*-muconate by a PCA 3,4-dioxygenase (PCD<sub>3,4</sub>), which is eventually converted to  $\beta$ KA by the sequential activities of 3-carboxy-*cis,cis*-muconate cycloisomerase, 4-carboxymuconolactone decarboxylase, and  $\beta$ -ketoadipate enol-lactone hydrolase (Harwood and Parales, 1996).

*P. putida*, that naturally employs the PCA 3,4-cleavage pathway, the most ubiquitous among bacteria, was engineered for the complete conversion of bis(2-hydroxyethyl) terephthalate (BHET) to  $\beta$ KA (Werner et al., 2021). The first step of this conversion involved BHET hydrolysis to mono(2-hydroxyethyl) terephthalate (MHET) and subsequent hydrolysis of the latter to TPA and EG. This was achieved by the incorporation of the *Ideonella sakaiensis* genes coding for PETase and MHETase, respectively. The second step of the overall conversion involved the genetic modification of the strain to facilitate TPA conversion to PCA, which was achieved by utilizing the TphA<sub>abc</sub> TPADO and the TphB DCD dehydrogenase from *Comamonas*, together with the TpaK transporter from *Rhodococcus jostii* for active membrane transport of TPA. Interestingly, the supplementation of BHET cultures with an additional 3.6 g/L glucose every 24 h—initially containing BHET and glucose in a 7:10 ratio—led to complete hydrolysis of BHET and substantially reduced MHET accumulation. Subsequently, to enable BHET conversion to  $\beta$ KA, *pcaIJ* encoding the 3-oxoadipate CoA-transferase was deleted, generating the final strain *P. putida* AW165. When this engineered strain was cultivated in a pH-controlled bioreactor supplied with BHET for 96 h, 32 g/L BHET were converted to about 15 g/L  $\beta$ KA, with a molar yield of 76 % and a productivity of 0.16 g  $\beta$ KA/L/h. Interestingly, in the proof-of-concept phase where chemocatalytic glycolysis of PET resulted in BHET and MHET, the conversion of the latter to  $\beta$ KA reached only 45 % molar yield. This reduced  $\beta$ KA production was associated with a pH decrease and was, thus, attributed to levulinic acid catabolism—a product of  $\beta$ KA decarboxylation below pH 7.0 (Werner et al., 2021).

In another study, *E. coli* was genetically engineered to enable both TPA degradation and  $\beta$ KA synthesis, with the latter proceeding via catechol and its ortho-cleavage pathway that merges with the PCA 3,4-cleavage pathway at the level of  $\beta$ -ketoadipate enol-lactone. The TPA degradation module, comprising *tphAabc* and *tphB* from *Comamonas* sp. E6, was incorporated in one vector, while another vector was coding for the AroY PCA decarboxylase from *K. pneumoniae*, leading to catechol formation. The third vector included the *P. putida* KT2440 cat operon genes (*catabc*) together with *pcaD* from *P. putida*, responsible for enol-lactone hydrolysis to  $\beta$ -KA (Harwood and Parales, 1996). Utilizing glycerol as the primary carbon source, this engineered *E. coli*  $\beta$ KA strain exhibited efficient TPA conversion to  $\beta$ KA achieving 98 % molar yield, albeit slow metabolism of glycerol and accumulation of acetic acid—a deleterious factor for TPA conversion—were observed. Higher oxygen

supply and regulation of acetic acid formation by *poxB* gene deletion—PoxB catalyzes the irreversible conversion of pyruvate into acetic acid—led to improved growth rates. Eventually, a two-stage bioconversion process was established for *E. coli*  $\beta$ KA  $\Delta$ *poxB* strain, consisting of the growth phase at pH 7.0, followed by the  $\beta$ KA production phase at pH 5.5. A total of 13.6 mM  $\beta$ KA was successfully produced with 96 % conversion efficiency (You et al., 2023).

### 3.2.4. Lycopene synthesis

Lycopene biosynthesis proceeds either via the 2-C-methyl-D-erythritol-4-phosphate (MEP) pathway found in prokaryotes (Fig. 2, Pathway D), or the mevalonate pathway operative in eukaryotes, such as yeasts and filamentous fungi. Both pathways converge to produce the precursors of lycopene, i.e., isopentenyl pyrophosphate (IPP) and dimethylallyl pyrophosphate (DMAPP) (Xu et al., 2021). In the MEP pathway, lycopene synthesis begins with the condensation of the key glycolytic intermediates, glyceraldehyde 3-P (G3P) and pyruvate, and continues in a nearly linear pathway. G3P and pyruvate are condensed to form 1-deoxy-d-xylulose-5-phosphate (DXP)—a reaction catalyzed by DXP synthase (DXS)—which is then converted to MEP by DXP reductoisomerase (DXR or IspC). A series of enzymes, namely 4-diphosphocytidyl-2C-methyl-d-erythritol cytidyltransferase (IspD) and kinase (IspE), 2C-methyl-d-erythritol-2,4-cyclodiphosphate synthase (IspF), 4-hydroxy-3-methyl-2-(*E*)-butenyl-4-diphosphate (HMBPP) synthase (IspG), and HMBPP reductase (IspH), successively catalyze the conversion of MEP to IPP, along with the respective intermediates. Subsequently, isopentenyl-diphosphate isomerase (IDI) catalyzes the isomerization of IPP to DMAPP, that are eventually condensed into geranyl diphosphate (GPP). GPP is converted to farnesyl pyrophosphate (FPP) by FPP synthase (IspA), followed by successive catalysis by geranylgeranyl diphosphate synthase (CrtE), phytoene synthase (CrtB), and phytoene desaturase (CrtI) to ultimately yield lycopene (Wang et al., 2020b).

The TCA cycle plays both catabolic and anabolic roles by oxidizing acetyl-CoA to CO<sub>2</sub> for ATP production and supplying precursor metabolites and NADPH for biosynthesis. In the absence of glucose, sugar biosynthesis from TCA intermediates is essential for growth, requiring phosphoenolpyruvate (PEP) carboxykinase to convert oxaloacetate to phosphoenolpyruvate. The metabolic link between glycolysis, gluconeogenesis, and the TCA cycle is centered on the PEP-pyruvate-oxaloacetate node, also known as the anaplerotic node (Alteri et al., 2009; Basu et al., 2018; Marrero et al., 2010; Sauer and Eikmanns, 2005). Therefore, assimilated carbon, upon entering the TCA cycle, can be redirected towards gluconeogenesis under specific metabolic conditions.

Several *Rhodococcus* sp. strains possess the complete enzymatic machinery for lycopene biosynthesis, with *R. jostii* strain RPET (RPET) is also capable of growing using PET hydrolysates as the sole carbon source. WT RPET cultures, fed with equimolar concentrations of TPA and EG, produced three unknown carotenoids and lycopene at low concentrations. Informed by the case of *Corynebacterium glutamicum*, where overexpression of CrtE, CrtB, and CrtI enhanced the flux from the precursor molecules towards lycopene, the RPET strain was metabolically engineered to incorporate the synthetic operon *crtEBI* (Henke et al., 2016). Indeed, the RPET engineered strain achieved lycopene synthesis of 630  $\mu$ g/L, a 300-fold improvement over the WT, all the while the previously observed unknown carotenoids were substantially decreased, suggestive of competing mechanisms to lycopene biosynthesis. Another approach focused on the supply increase of the precursors IPP and DMAPP through the modification of their biosynthetic pathway. A synthetic *dxs-idi* operon, coding for the enzymes DXS and IDI, was expressed in RPET leading to a 390-fold augmentation of lycopene production (817  $\mu$ g/L). However, the co-expression of *crtEBI* and *dxs-idi* had no cumulative effect but, instead, resulted in slightly lower yields compared to each individual approach (606  $\mu$ g/L). The feasibility of upcycling PET into value-added chemicals was validated by exploring

lycopene production by the engineered RPET strain with 10 % v/v PET hydrolysates—resulting from alkaline hydrolysis—as the sole carbon source. The culture achieved a final lycopene titer of 1.2 mg/L, which improved to 1.3 mg/L in fed-batch fermentations (Diao et al., 2023).

### 3.2.5. Biopolymers synthesis

**3.2.5.1. PHAs.** The soil-isolated *Pseudomonas* strains, *P. putida* GO16, *P. putida* GO19, and *P. frederiksborgensis* GO23, were found to metabolize TPA as a sole carbon and energy source, while, simultaneously, accumulating mcl-PHAs at 23–27 % of their total cell dry weight (CDW) after 48 h. All three strains converted TPA to PHAs, but with varying efficiencies and polymer properties. Strain GO19 had the highest conversion efficiency, producing 8.4 mg/L/h of PHA. GO16 and GO19 showed higher PHA accumulation rates, though these were short-lived. Strain GO23, despite a lower initial rate, sustained its accumulation longer, making it potentially more suitable for industrial applications. GO16 and GO19 mainly produced 3-hydroxydecanoic acid polymers, while GO23 also synthesized 3-hydroxydodecanoic acid and 3-hydroxydodecenoic acid. All strains produced small amounts of 3-hydroxyhexanoic acid and 3-hydroxyoctanoic acid (Kenny et al., 2008).

Building upon the insights from shaken flask experiments, fed-batch fermentations with *P. putida* GO16 were optimized to enhance the conversion of TPA to PHAs. When TPA was the sole carbon source, *P. putida* GO16 achieved a CDW of 8.7 g/L and a PHA concentration of 2.6 g/L within 48 h, with PHA reaching 30 % of the CDW. The PHA produced was primarily composed of 3-hydroxydecanoic acid, though with a reduced proportion of 3-hydroxydodecenoic acid. Interestingly, continuous but decreasing nitrogen supply throughout the fermentation, instead of the conventional nitrogen limitation approach, led to a biomass yield of 0.6 g/g TPA, a PHA yield of 0.2 g/g TPA, and a 10-fold increase of PHA productivity (0.05 g/L/h) for *P. putida* GO16. On the other hand, when waste glycerol was supplied as the sole carbon source, *P. putida* GO16 utilized 222 g of the substrate, resulting in the accumulation of 108.9 g of biomass and 35.6 g of PHA over 48 h; the produced PHAs were primarily composed of C<sub>8</sub>, C<sub>10</sub>, and C<sub>12</sub> monomers. In experiments where TPA and waste glycerol were co-supplied at the same ratio, the molecular weight of the PHAs decreased, and the monomer composition shifted to include higher proportions of C<sub>12</sub> and C<sub>14</sub> monomers, particularly 3-hydroxytetradecanoic acid and 3-hydroxytridecanoic acid, which were absent when TPA was the sole carbon source. Mixed substrate fermentations with waste glycerol and TPA improved both biomass accumulation and PHA productivity compared to TPA alone, leading to a 1.2-fold increase in TPA utilization, a 1.6-fold rise in biomass productivity, and a 2-fold boost in PHA productivity, suggesting that co-feeding strategies could generally enhance productivity in similar cases (Kenny et al., 2012).

Another study evaluated the PHAs synthesis potential of *Pseudomonas umsongensis* GO16 KS3—a strain adapted through adaptive laboratory evolution (ALE) to grow on EG—when grown on enzymatically hydrolyzed amorphous PET films with a 47 % degree of depolymerization (Tiso et al., 2021). Remarkably, complete TPA consumption occurred within 23 h while EG was depleted at a 3.5-fold slower rate. After nitrogen depletion, PHA accumulation reached 7 % of CDW, with a biomass yield of 0.2 g CDW/g substrate and a PHA yield of 0.014 g /g substrate, with mcl-PHAs composed of C<sub>8</sub>, C<sub>10</sub>, and C<sub>12</sub> monomers. Subsequently, *P. umsongensis* GO16 KS3 was engineered with the 3-(3-hydroxyalkanoyloxy) alkanolic acid synthesis plasmid pSB01 (Tiso et al., 2017a), enhancing the expression of RhlA, a 3-hydroxyacyl-ACP-O-3 hydroxyacyltransferase that catalyzes the formation of 3-(3-hydroxyalkanoyloxy) alkanolic acid by linking two activated  $\beta$ -hydroxy fatty acids. The engineered strain synthesized 3-(3-hydroxyalkanoyloxy) alkanolic acid exclusively from TPA, achieving a production rate of 5 mg/L/h and a yield of 0.01 g 3-(3-hydroxyalkanoyloxy) alkanolic acid /g TPA, while EG apparently only supported growth (Tiso et al., 2021).

Another *Pseudomonas* strain isolated from PET waste, *P. stutzeri* TPA3, was able to catabolize TPA, but didn't naturally accumulate any form of PHA. This strain was found to harbor the necessary genes for TPA conversion to PCA, which is subsequently metabolized into succinyl-CoA and acetyl-CoA through the  $\beta$ KA pathway (Harwood and Parales, 1996). By introducing the *phbCAB* operon from *Ralstonia eutropha*, responsible for the conversion of acetoacetyl-CoA to P3HB, engineered *P. stutzeri* TPA3P produced pure P3HB from TPA; notably, PhbC from *R. eutropha* is exclusively synthesizing scl-PHAs (Li et al., 2011). This engineered strain accumulated P3HB up to 12 % of CDW, when grown on 10 g/L TPA as the sole carbon source (Liu et al., 2021).

Beyond pseudomonads, the bacterial strain *I. sakaiensis* 201-F6, renowned for its PET-degrading capability, was found to possess a *phaCAB* gene cluster, suggesting PHAs production. When *I. sakaiensis* 201-F6 was cultured with PET granules, a high growth was observed, achieving a DCW of up to 1.6 g/L, demonstrating that PET served as a carbon source. The low concentration of PET hydrolysates in the culture supernatant compared to the PET weight loss suggests a rapid uptake of these degradation products by the cells. After 6 days of incubation, *I. sakaiensis* accumulated PHAs accounting for 48 % w/w of the DCW. However, 9 % of the carbon from PET was converted to PHAs, with the majority being metabolized into other compounds, including CO<sub>2</sub>. The predominant monomer detected was methyl-3HB, comprising approximately 100 mol%, along with trace amounts of methyl 3-hydroxyvalerate, indicating that the synthesized PHA was nearly a P3HB homopolymer. Cultivation of *I. sakaiensis* 201-F6 with the PET degradation monomers TPA and EG, resulted in reduced growth and P3HB production (<5 %), indicating the strain preferentially utilizes PET hydrolytic oligomers over the individual monomers for growth and PHA synthesis (Fujiwara et al., 2021).

**3.2.5.2. Bacterial nanocellulose.** BNC is an extracellular biopolymer that forms a three-dimensional network at the air-liquid culture medium interface, and at least one of its dimensions is less than or equal to 100 nm. BNC bacterial production is closely related to many metabolic pathways, such as the pentose-phosphate pathway, the Embden–Meyerhof–Parnas pathway, the TCA cycle, and gluconeogenesis. BNC biosynthesis requires glucose-6-phosphate (Glu-6-P) as its main precursor, which could result from various routes, such as direct glucose assimilation, fructose metabolism, or the intracellular cascade of TCA cycle-pyruvate-gluconeogenesis. Once at the level of Glu-6-P, the BNC pathway proceeds via three chemical conversions (Fig. 2, Pathway F). Isomerization of Glu-6-P by phosphoglucosyltransferase (PGM) yields glucose-1-phosphate (Glu-1-P), which is then converted to uridine diphosphate glucose (UDP-Glu) by UDP-Glu pyrophosphorylase; UDP-Glu is then polymerized by cellulose synthase (Bcs) into linear 1,4 glucan chains, which are activated by cyclic diguanylate (di-GMP) (Barja, 2021). In *Komagataeibacter xylinus*, Bcs function depends on the *bcsABCD* operon, where *bcsA* codes for the catalytic subunit and *bcsB* for a regulatory subunit that binds to cyclic di-GMP, while the roles of *bcsC* and *bcsD* are not yet fully understood (Ross et al., 1991).

Two *K. xylinus* strains, i.e., DSM 2004 and DSM 46604, were screened for their ability to produce BNC upon cultivation on TPA and/or EG. Both strains were able to utilize the mixture of TPA and EG as carbon source and produce BNC, although with different yields and variations in their crystallinity and nanostructure. *K. xylinus* DSM 2004 achieved higher BNC production from TPA (0.8 g/L), EG (0.6 g/L), and TPA/EG mixtures (0.6 g/L) than strain DSM 46604. The latter was unable to utilize EG as the sole carbon source but reached BNC production of 0.2 g/L both from TPA and the mixture (Esmail et al., 2022).

### 3.3. Ethylene glycol

#### 3.3.1. Glycolate and its assimilation

During aerobic metabolism, the assimilation of EG proceeds via the

intermediate glycolaldehyde, which can be assimilated through various natural and synthetic pathways. EG is oxidized to glycolaldehyde (Fig. 3) by two functionally redundant periplasmic pyrroloquinoline quinone-dependent alcohol dehydrogenases (PedE and PedH) in *Pseudomonas* or by a 1,2-propanediol oxidoreductase (FucO) in *E. coli*, followed by the conversion to glycolate by cytoplasmic aldehyde dehydrogenases (PP\_0545, PedI, and AldA). Some microorganisms can further oxidize glycolate to glyoxylate by the membrane anchored glycolate oxidase GlcDEF, and the latter can shortly enter the TCA cycle via either ligation with acetyl-CoA by malate synthase (GlcB) for the formation of malate, or condensation with succinate by isocitrate lyase (AceA) for the formation of isocitrate (Frandsen et al., 2018).

Several WT yeasts from the genera *Saccharomyces*, *Pichia*, *Hansenula*, and *Yarrowia lipolytica* have demonstrated the ability to perform oxidative biotransformation of EG to glycolate. The highest yield among the yeasts was observed by *Y. lipolytica* IMUFRJ 50682, that was capable of glycolate production, uncoupled to cell growth metabolism, at a molar yield of 86 % from 0.5 M EG; interestingly, this strain appeared tolerant up to 2 M EG titers (Carniel et al., 2023). *Pichia naganishii* AKU 4267 produced 35.3 g/L from 10 % v/v EG, achieving a molar conversion yield of 26 %. After optimizing the culture conditions, the yield increased to 88 % after 120 h, with complete substrate consumption, no intermediate accumulation, and the production of 150 g/L glycolate. However, when 20 % v/v EG was utilized, the yield dropped to 12 % (Kataoka et al., 2001).

The ability of *Gluconobacter* to convert EG to glycolate was also evaluated in various strains of *G. oxydans*, with *G. oxydans* DSM 2003 converting 70 g/L EG to 70.2 g/L glycolate after 48 h, with a molar conversion yield of 87 % and no detection of by-products (Wei et al., 2009). *G. oxydans* KCCM 40109 outperformed the previous, utilizing EG derived from microwave-radiated depolymerized PET, and achieving a maximum molar yield of 99 % with 10.7 mM EG within 12 h (Kim et al., 2019).

Soil-isolated microorganisms *Rhodotorula* sp., *Cryptococcus* sp., and *Burkholderia* sp. EG13 were also capable of growing on EG and producing glycolate, with molar conversion yields above 10 %. *Rhodotorula* sp. 3Pr-126 initially achieved a molar yield of 19 %, which was improved to 92 % after culture optimization. As a result, 110 g/L glycolate was produced after 120 h, with complete EG consumption and no intermediate accumulation. However, when the EG supply was doubled, i.e., 20 % v/v, the molar yield was 3-fold lower (Kataoka et al., 2001). *Burkholderia* sp. EG13 produced glycolate with a yield of 99 % from 200 mM EG after 24 h. To enhance production, in-situ product removal using adsorptive biotransformation was implemented, accumulating 793 mM glycolate after the fourth feed, in a 5-L bioreactor with a 2-L working volume (Gao et al., 2014).

In addition to utilizing native systems, synthetic biology has increasingly focused on engineering model organisms to assimilate EG and convert it to glycolate. By fine-tuning factors like oxygen concentration, researchers have achieved significant yields, demonstrating the potential of using EG as a renewable substrate for producing valuable chemicals. *E. coli* MG1655 was engineered for overexpression of its own 1,2-propanediol oxidoreductase FucO—also mutated to confer oxygen-resistance—and aldehyde dehydrogenase AldA, since the WT strain is not able to efficiently metabolize EG, despite harboring the genes for the purpose. The engineered strain could, indeed, convert EG to glycolate, and while under aerobic conditions glycolate oxidation to glyoxylate by native glycolate oxidase supported growth, under oxygen-limiting conditions glycolate accumulated as a product. In bioreactor fermentations with aeration control, glycolate production began after 28 h and continued until fermentation was terminated. Over a 112-h production period, a total of 10.4 g/L glycolate was generated, with an overall yield of 0.8 g/g EG and a productivity of 0.1 g/L/h (Pandit et al., 2021).

### 3.3.1.1. Glyoxylate carboligase pathway. An alternative catabolic route

for glycolate is the glyoxylate carboligase (gcl) pathway (Fig. 3, Pathway A), through which two molecules of glyoxylate are condensed by Gcl to form tartronic semialdehyde, that is further reduced to glycerate, either directly by a tartronate semialdehyde reductase (GlxR) or via the hydroxypyruvate intermediate—hydroxypyruvate isomerase (Hxi) and hydroxypyruvate reductase (TtuD) catalyze the consecutive reactions within. Eventually, glycerate is phosphorylated by glycerate kinase to give either of two glycolytic intermediates, glycerate 3-phosphate or the 2-phospho isomer, which either proceed to glycolysis or participate in gluconeogenesis, depending on the cellular needs (Pandit et al., 2021).

Mückschel and coworkers (Mückschel et al., 2012), studied EG assimilation by two *P. putida* strains. *P. putida* JM37 was able to fully convert 50 mM EG within 24 h, with no detectable intermediates. *P. putida* KT2440, however, was unable to grow on EG and required over 48 h for complete EG conversion, during which glycolate, glyoxylate, and oxalate were identified in the supernatant. Proteomics analyses revealed that both strains induced the expression of PedI that is responsible for glycolaldehyde conversion to glycolate. However, *P. putida* JM37 additionally expressed Gcl, GlcB, and AceA that leads to the incorporation of glyoxylate into the TCA cycle via the glyoxylate shunt, thus facilitating growth.

Another study utilized ALE on *P. putida* KT2440 and the resulting strains successfully grew on EG. Interestingly, they all exhibited mutations in the *gclR* gene, which encodes a putative GntR-type transcriptional regulator responsible for repressing the *gcl* pathway. Interestingly, a few strains also exhibited mutations in the gene with locus tag PP\_2046, encoding a LysR-type transcriptional regulator likely involved in controlling the adjacent operon that encodes enzymes pertinent to  $\beta$ -oxidation. Additionally, mutations were identified in the PP\_2262 locus tag, which encodes a putative porin located upstream of an operon associated with a two-component sensory system. To evaluate the functional significance of these mutations, reverse engineering was performed on the parental KT2440 strain. Notably, deletion of the *gclR* gene enabled growth on EG, while simultaneous deletion of both PP\_2046 and PP\_2262 genes resulted in the fastest growth rates and the highest final biomass production. The absence of significant growth differences upon the deletion of either PP\_2046 or PP\_2262 suggests a complex interplay between these secondary mutations, likely influencing the balance between substrate transport across the outer membrane and the oxidation of alcohols and aldehydes (Li et al., 2019).

Unlike conventional approaches that rely on a single microorganism for PET upcycling, emerging strategies explore the use of microbial consortia to enhance degradation and assimilation processes. To address the limitations of individual strains, a four-species microbial consortium was designed to enhance PET breakdown by alleviating the inhibitory effects of its degradation products. Two strains of *B. subtilis* 168 were modified to secrete the enzymes PETase and MHETase, enabling PET hydrolysis into TPA and EG, respectively. *R. jostii* RHA1 and *P. putida* KT2440—capable of assimilating TPA and EG, respectively—were also introduced to alleviate the inhibitory effect of the PET monomers on the depolymerizing process. Through optimization of environmental conditions and inoculation ratios, the consortium achieved a PET depolymerization rate of 23 % in seven days – an improvement of 71 % compared to the degradation achieved by *Bacillus* strains alone. Although this study does not focus on producing high-value products, it demonstrates the potential of artificial microbial consortia in both PET depolymerization and monomer assimilation, offering insights into future strategies in plastic waste valorization (Qi et al., 2021).

Another recent study explored the upcycling potential of a microbial consortium consisting of two *P. putida* strains: Pp-T, specializing in TPA assimilation, and Pp-E, in EG utilization (Bao et al., 2023). Pp-T was derived from EM42 by deleting the *pedEHI* gene cluster to prevent EG oxidation to glycolate and introducing the *tpa* gene cluster from *R. jostii* RHA1 for TPA conversion to PCA (Section 3.2.1). Pp-E was constructed from M31 by: (i) deleting the *gclR* gene, encoding a transcriptional



regulator responsible for repressing the *gcl* pathway, and (ii) replacing the native promoter of the glycolate oxidase (*gclDEF*), yielding glyoxylate, with a strong *P*<sub>tac</sub> promoter to enhance EG assimilation. The Pp-T/Pp-E consortium depleted 75 mM each TPA and EG in 62 h, outperforming the single-engineered Pp-TE strain, and also completely processed crude PET hydrolysates containing 50 mM each TPA and EG.

To further enhance PET hydrolysate upcycling, the study implemented the “division of labor” approach for the Pp-TC/ Pp-EM consortium aiming at MA biosynthesis. Pp-TC could convert TPA to catechol, and Pp-EM could convert catechol to MA while consuming EG. Pp-TC was engineered by deleting the *catRBCA* cluster to block the main catechol catabolic pathway and introducing the codon-optimized PCA decarboxylase *aroY* (Section 3.2.1) and the *E. cloacae* decarboxylase enhancer *ecdB* for catechol conversion. Pp-EM was engineered by deleting the *catRBC* operon and enhancing the conversion of catechol to MA with a *P*<sub>tac</sub> promoter for the *catA* gene. The Pp-TC/ Pp-EM consortium, with a 1:5 inoculation ratio and optimized fermentation conditions, reached a molar yield of 33 % MA from PET hydrolysates containing 50 mM each TPA and EG, outperforming previous methods and single-strain systems (Bao et al., 2023). Although optimization could further develop this process, especially in terms of PET hydrolysate toxicity effects, this study established an integrated deconstruction process from powdered plastic to microbial biomass, demonstrating the engineered consortium’s high substrate conversion efficiency.

**3.3.1.2.  $\beta$ -hydroxyaspartate cycle.** The assimilation of EG in *P. putida* via the *gcl* pathway is constrained by the *gcl* reaction, which catalyzes the condensation of two glyoxylate molecules into tartronate semialdehyde, leading to CO<sub>2</sub> release and reduced carbon efficiency (Kaplun et al., 2008). To improve EG assimilation, an alternative glyoxylate assimilation pathway with enhanced carbon retention was explored. The  $\beta$ -hydroxyaspartate cycle (BHAC), originally described in the 1960s (Kornberg and Morris, 1963) and recently fully characterized in *Paracoccus denitrificans* (Schada von Borzyskowski et al., 2019), provides a more carbon-efficient alternative by converting two glyoxylate molecules into oxaloacetate without CO<sub>2</sub> release. The cycle begins with aspartate-glyoxylate aminotransferase (BhcA), a pyridoxal 5'-phosphate-dependent enzyme that transaminates glyoxylate into glycine, using aspartate as the preferred amino donor. The key step is then catalyzed by  $\beta$ -hydroxyaspartate aldolase (BhcC), which facilitates the condensation of glyoxylate and glycine to form  $\beta$ -hydroxyaspartate. This intermediate is subsequently dehydrated by  $\beta$ -hydroxyaspartate dehydratase (BhcB) to yield iminosuccinate, which is then reduced to L-aspartate by iminosuccinate reductase (BhcD), completing the cycle (Fig. 3, Pathway J). By implementing the BHAC into *P. putida* KT2440 and applying ALE, the resulting strain KT2440  $\Delta$ *gcl* + BHAC exhibited enhanced growth rate and biomass yield on EG (Schada von Borzyskowski et al., 2023), outperforming previous *P. putida* strains utilizing the glycerate pathway (Franden et al., 2018; Li et al., 2019).

**3.3.1.3. Tartronyl-CoA pathway.** The tartronyl-CoA (TaCo) pathway was recently proposed as a synthetic route for glycolate assimilation into central metabolism, designed to incorporate CO<sub>2</sub> rather than releasing it. While theoretically more carbon-efficient than natural glycolate assimilation routes, the pathway remained speculative, as neither tartronyl-CoA nor its associated enzymatic reactions had been observed in nature. To realize this pathway, Scheffen et al., engineered a novel glycolyl-CoA carboxylase through rational design, high-throughput microfluidics, and microplate screening (Scheffen et al., 2021). This enzyme catalyzes the carboxylation of glycolyl-CoA to tartronyl-CoA, which is subsequently reduced to glycerate by a tartronyl-CoA reductase from *Chloroflexus aurantiacus* (Fig. 3, Pathway L). A TaCo-based route for EG assimilation was then constructed to enhance carbon efficiency. This pathway integrated: (i) an alcohol dehydrogenase from *G. oxydans* (Gox0313) for EG conversion to glycolaldehyde, (ii) an

aldehyde dehydrogenase from *Rhodospseudomonas palustris* BisB18 (PduP) for glycolyl-CoA formation, (iii) the newly developed glycolyl-CoA carboxylase, (iv) the *C. aurantiacus* tartronyl-CoA reductase, and (v) other genetic modifications that enhanced ATP and NAD<sup>+</sup> regeneration. This system served as a proof of principle and produced approximately 500  $\mu$ M glycerate from 119 mM EG within 2 h.

**3.3.1.4. D-arabinose 5-phosphate-dependent glycolaldehyde assimilation pathway.** The intracellular assimilation of EG proceeds via the intermediate glycolaldehyde. However, naturally occurring pathways for glycolaldehyde assimilation exhibit low carbon efficiency in producing acetyl-CoA. A recently designed and in vitro validated pathway enabling carbon-conserving glycolaldehyde conversion to acetyl-CoA (Yang et al., 2019) was implemented in vivo to enhance EG assimilation (Wagner et al., 2023).

This synthetic glycolaldehyde assimilation pathway comprises one heterologous enzyme and engineered endogenous *E. coli* enzymes, overexpressed in the host strain *E. coli* MG1655  $\Delta$ yqhD  $\Delta$ aldA *lacI*q, where genes encoding the major glycolaldehyde reductase YqhD (Alkim et al., 2015) and glycolaldehyde dehydrogenase AldA (Cam et al., 2016) were deleted to promote synthetic pathway utilization. The pathway initiates with FucO, yielding glycolaldehyde (Pandit et al., 2021). Subsequently, fructose 6-phosphate aldolase (FsaA) catalyzes the aldol addition of glycolaldehyde to glyceraldehyde 3-phosphate, forming D-arabinose 5-phosphate (Ara5P). Ara5P is then converted to D-xylulose 5-phosphate (Xylu5P) via Ara5P isomerase (KdsD) and D-ribulose 5-phosphate 3-epimerase (Rpe). Finally, *Clostridium acetobutylicum* phosphoketolase (CaPkt) converts Xylu5P into acetyl phosphate, which is further metabolized into acetate (Fig. 3, Pathway I).

The resulting engineered *E. coli* EG4 strain, overexpressing all pathway enzymes except Rpe, facilitated EG conversion to acetyl phosphate but exhibited minimal acetate accumulation (0.096 mM from 500 mM EG), likely due to thermodynamic constraints limiting downstream flux. To support growth, glycerol was used as a co-substrate, as it leads to lower acetate production compared to glucose (Martínez-Gómez et al., 2012). Although the observed yields remain low, this study demonstrates the feasibility of the Ara5P-dependent glycolaldehyde assimilation pathway under EG-utilizing conditions, paving the way for alternative assimilation routes that integrate into central metabolism and may be coupled to value-added product biosynthesis.

### 3.3.2. 2,4-dihydroxybutyric acid

Based on the concept of glycolaldehyde serving as a metabolic hub, channeling carbon sources into central cellular metabolism, another synthetic modular EG-assimilating glycolaldehyde-dependent pathway has been designed, this time coupled with the production of DHB (Frazão et al., 2023). This non-natural pathway proceeds via the NAD<sup>+</sup>-dependent alcohol dehydrogenase from *G. oxydans* Gox0313 (Scheffen et al., 2021) that catalyzes EG conversion to glycolaldehyde. Two molecules of glycolaldehyde are then converted into DHB by five consecutive reaction steps. In the first step, two molecules of glycolaldehyde are fused by the action of the *E. coli* D-threose aldolase Ec.FsaATA (Szekrenyi et al., 2014), to yield a single D-threose molecule. The resulting four-carbon sugar is oxidized by the *Paraburkholderia caryophylli* D-threose dehydrogenase Pc.TadH (Sasajima and Sinskey, 1979), to D-threono-1,4-lactone, which can then be converted to the corresponding sugar acid either spontaneously or in a reaction catalyzed by the *Thermogutta terrifontis* D-threono-1,4-lactonase Tt.Lac11 (Westlake, 2019). In the last two reaction steps, D-threonate is first dehydrated to 2-oxo-4-hydroxybutyrate by the *Herbaspirillum huttiense* D-threonate dehydratase Hh.AraD (Yew et al., 2006), and then the latter is reduced to yield DHB in a reaction catalyzed by the *E. coli* 2-oxo-4-hydroxybutyrate reductase Ec.Mdh5Q (quintuple mutant) (Fig. 3, Pathway K) (Frazão et al., 2018).

Following enzyme screening and transport optimization, Frazão and



coworkers (Frazão et al., 2023) developed *E. coli* TW354, which produced 6.8 mM DHB from EG via glycolaldehyde, albeit with low rates and titers (2 % molar yield). While further optimization is required to enhance efficiency, this study demonstrates a promising strategy for converting EG into valuable compounds, contributing to synthetic pathway design for improved CO<sub>2</sub> utilization.

### 3.3.3. Aromatics

Subsequent studies on *E. coli* MG1655, which enabled EG conversion to glycolate (Section 3.3.1), led to the development of *E. coli* EGT01. This strain was engineered for (i) enhanced EG utilization through FucO (Pandit et al., 2021) and (ii) L-tyrosine overproduction via two gene deletions and the incorporation of pTYR01 plasmid, which overexpresses feedback-resistant *aroG* and *tyrA* under a lac promoter. Medium optimization and process engineering enabled *E. coli* EGT01 to convert 270 mM EG into L-tyrosine at a molar yield of 6 %, surpassing glucose under comparable conditions (Panda et al., 2023). Using similar strategies, the same authors engineered *E. coli* EGP01 and EGC02, achieving phenylalanine and p-coumaric acid production at molar yields of 5.7 % and 3.8 %, respectively, from 160 mM EG. Finally, EG derived from waste PET hydrolysates supported L-tyrosine biosynthesis at yields comparable to commercial EG, demonstrating the potential of these engineered strains for PET upcycling.

Comparative transcriptome analysis provided insights into the metabolic pathway enabling EG conversion to L-tyrosine in *E. coli* EGT01 (Panda et al., 2023). EG is initially oxidized to glycolaldehyde and glycolate by the 1,2-propanediol oxidoreductase FucO and the aldehyde dehydrogenase AldA, respectively. Glycolate is further oxidized to glyoxylate by glycolate oxidase (GlcDEF) and enters the *gcl* pathway, eventually leading to the formation of 2-phosphoglycerate. Enolase (Eno) then catalyzes its dehydration to PEP, a key precursor in the shikimate pathway. In this pathway, PEP condenses with erythrose-4-phosphate, a pentose phosphate pathway intermediate, to form 3-deoxy-D-arabino-heptulosonate 7-phosphate (DAHP), catalyzed by DAHP synthases (e.g., AroG). DAHP undergoes six enzymatic transformations to chorismate, which is decarboxylated to 4-hydroxyphenylpyruvate by the bifunctional chorismate mutase/prephenate dehydrogenase TyrA. Finally, 4-hydroxyphenylpyruvate is transaminated to L-tyrosine using L-glutamate as the amino donor (Fig. 3, Pathway H) (Bentley and Haslam, 1990).

### 3.3.4. Anaerobic acetogenic pathway

In the acetogenic bacterium *Acetobacterium woodii*, the working hypothesis for EG metabolism comprises EG dehydration to acetaldehyde (Fig. 3, Pathway B) by a propane diol dehydratase (PduCDE)—the only dehydratase expressed in EG-growing cells—and then dismutation to ethanol and acetyl-CoA by a CoA-dependent propionaldehyde dehydrogenase (PduP) (Trifunović et al., 2016). Acetyl-CoA is further converted to acetate with concomitant ATP formation by substrate-level phosphorylation, while ethanol is oxidized to acetate, while the reducing equivalents are recycled by reduction of CO<sub>2</sub> to acetate via the reductive acetyl-CoA pathway (i.e., the Wood-Ljungdahl pathway) (Trifunović et al., 2016).

### 3.3.5. PHAs synthesis

*P. putida* KT2440 has the necessary genetic inventory that would enable utilization of EG as a sole carbon source for growth via the *gcl* pathway (Fig. 3, Pathway A), but expression is, apparently, not induced under relevant conditions. One study focused on engineering *P. putida* KT2440 to efficiently metabolize EG and produce mcl-PHAs, by overexpressing the complete *gcl* operon, coding for the glycolate oxidase GlcDEF that yields glyoxylate, and the other necessary enzymes for the downstream conversion of glyoxylate to glycolytic intermediates (Section 3.3.1.1). The engineered *P. putida* MFL185 strain demonstrated the ability to grow on EG concentrations as high as 2 M and completely metabolized up to 500 mM EG within 120 h. When supplied with 100

mM EG as the sole carbon source, MFL185 produced mcl-PHAs constituting 32 % DCW, with a product yield of 0.06 g/g and most of the monomers being C<sub>8</sub> and C<sub>10</sub> (Frandsen et al., 2018). ALE was also successful when performed on *P. umsongensis* GO16, resulting in the KS3 strain that could grow on EG as the sole carbon source. Additionally, when PET hydrolysates were fed to the evolved strain, PHA production associated with both EG and TPA was detected, although further detailed studies on EG utilization for PHA synthesis are deemed necessary (Tiso et al., 2021).

In a recent study, *P. putida* strains Pp-T, Pp-E and Pp-TEP were engineered for enhanced mcl-PHAs production from PET-derived substrates by overexpression of key PHA biosynthetic genes (*phaG*, *alkK*, *phaC1*, *phaC2*) under the control of a constitutive promoter (Bao et al., 2023). The resulting strains, designated Pp-TP, Pp-EP, and Pp-TEP, demonstrated significant mcl-PHA yields, with Pp-TP producing 164 mg/L, Pp-EP 31 mg/L, and Pp-TEP 128 mg/L mcl-PHAs, during TPA and EG fermentation. In fermentations using PET hydrolysate containing 50 mM each TPA and EG, the TP/EP consortium consumed all hydrolysate in 65 h and produced 296 mg/L of mcl-PHAs, while Pp-TEP left 82 % of EG unconsumed. In fed-batch fermentations, under the same hydrolysate concentration, the TP/EP consortium produced 637 mg/L of mcl-PHAs, a 92 % increase compared to Pp-TEP.

## 3.4. Lactic acid

### 3.4.1. Biopolymers synthesis

**3.4.1.1. PHAs.** *R. eutropha* is a model organism for PHA synthesis, as well as a major industrially important strain, as it can accumulate large amounts of intracellular PHAs under nutrient limitation. PHA production by *R. eutropha* generally occurs during the stationary phase, hence, cells are first grown to high density after which a key nutrient is limited to trigger PHA synthesis (Chakraborty et al., 2012; Huschner et al., 2015; Lee, 1996).

A strain of *R. eutropha* was investigated for its ability to grow and accumulate PHAs when provided with a medium containing acetic, butyric, lactic and propionic acids, and LA was shown to be rapidly consumed (Chakraborty et al., 2012). According to subsequent studies, the presence of both LA and acetic acid was crucial for *R. eutropha* growth and PHAs production. When these two organic acids were exclusively present in the culture medium, higher CDW and PHAs productivity were observed, reaching 75 g/L and 55 g/L, respectively (Huschner et al., 2015; Tsuge et al., 2001). *R. eutropha* NRRL B14690 was also investigated for its ability to produce P3HB when grown on LA. At concentrations of 20 g/L LA, the culture yielded 1.2 g/L biomass and 0.09 g/L P3HB. Despite yielding less than half the amount observed with fructose—the standard carbon source—LA emerged as the second most effective carbon source used for P3HB production, among the 13 different carbon sources tested (i.e., fructose, glucose, LA, xylose, sucrose, molasses, sorbose, acetic acid, starch, sodium acetate, glycerol, lactose and propionic acid) (Khanna and Srivastava, 2005).

Although P3HB has been studied for decades and is efficiently produced from renewable carbon sources, its range of applications is limited due to its brittleness, stiffness, and high melting point. However, when LA is polymerized with P3HB, forming the copolymer poly(3HB-co-LA), the mechanical properties, the flexibility, and the transparency of the biomaterial are greatly improved (Yamada et al., 2011).

*E. coli* XL-Blue was engineered to produce poly(3HB-co-LA) from glucose by enhancing both the biosynthesis and incorporation of lactyl-CoA into the copolymer. Key mutations in *Clostridium propionicum* propionate CoA-transferase (PctCp) produced enzymes (Pct532Cp and Pct540Cp) with improved lactyl-CoA production, increasing both polymer content and LA mole fraction in the copolymer. Moreover, site-directed mutagenesis of *Pseudomonas* PHA synthase (PhaC1 Ps6–19) enhanced lactate incorporation (Yang et al., 2010). The engineered

*E. coli* strain was able to synthesize pure PLA when no 3HB was supplied, while with increasing concentrations of 3HB supplied, a linear decrease of the LA fraction of the copolymer was observed.

The strain was further modified in a subsequent study, by knocking out the *ackA*, *ppc*, and *adhE* genes and replacing the native promoters of the *ldhA* and *acs* genes. The *ackA* and *adhE* genes encode for an acetate kinase and an acetaldehyde/alcohol dehydrogenase, responsible for acetate and ethanol formation from acetyl-CoA, respectively. Consequently, their deletion led to increased levels of acetyl-CoA, a major CoA donor for the generation of both lactyl-CoA and 3HB-CoA. The *ppc* gene encodes a pyruvate carboxylase, converting pyruvate to oxaloacetate, and its deletion increased the available pyruvate for lactate synthesis. Replacement of the native promoters of the *ldhA* (D-lactate dehydrogenase) and *acs* (acetyl-CoA synthetase) genes with the *trc* promoter, relieved the native regulation of genes expression and allowed higher lactate and acetyl-CoA formation, respectively. Introduction of *Cupriavidus necator* (widely known as *R. eutropha*) *phaA* and *phaB* genes, encoding  $\beta$ -ketothiolase and acetoacetyl-CoA reductase, respectively, allowed copolymer production without 3HB feeding. The final engineered *E. coli* JLX10 strain achieved LA fractions up to 70 mol% and polymer content of 20 % w/w (Jung et al., 2010). Based on this study, a fermentation setup where this, or a similarly performing bacterial strain, will be feeding on LA and producing P(3HB-co-LA), could be envisaged. For this to happen, LA oxidation to pyruvate by a lactate dehydrogenase (LDH) would be followed by conversion to acetyl-CoA by a pyruvate-ferredoxin oxidoreductase. Afterwards, any of the three primary metabolic pathways providing 3-hydroxyacyl precursors (Section 3.1) would result in copolymer production.

**3.4.1.2. Bacterial nanocellulose.** BNC biosynthesis depends on the Glu-6-P precursor and, thus, any carbon source that can be metabolized down to the level of Glu-6-P is a valid candidate for BNC production. Indeed, LA, being converted to pyruvate by LDH, can enter gluconeogenesis and eventually yield Glu-6-P (Fig. 3) (Hanson and Owen, 2004). A recent study reported PLA hydrolysates successfully supporting growth and BNC production by *Komagataeibacter medellinensis* ID13488 (Sourkouni et al., 2023). The valorization of PLA into BNC, through enzymatic hydrolysis and microbial fermentation, yielded varying amounts of LA, 30–70 % that from glucose, depending on the pretreatment method and duration.

### 3.4.2. Reverse $\beta$ -oxidation pathway

**3.4.2.1. Butyric acid.** Although there are butyrate-producing pathways where amino acids serve as major substrates, i.e., the lysine, glutarate, and 4-aminobutyrate pathways, the most prevalent bacterial pathway for butyrate production proceeds via acetyl-CoA and the reverse  $\beta$ -oxidation pathway (Fig. 3, Pathway C). According to this, the first key metabolic intermediate is acetyl-CoA, which, in this case, results from LA oxidation to pyruvate. Synthesis of butyryl-CoA proceeds via condensation of two acetyl-CoA molecules into acetoacetyl-CoA, reduction to 3-hydroxybutyryl-CoA, and dehydration to crotonyl-CoA. All four pathways merge at a central energy-generating step where crotonyl-CoA is reduced to butyryl-CoA by a butyryl-CoA dehydrogenase electron-transferring flavoprotein complex. Subsequently, butyryl-CoA is transformed to butyrate either by butyryl-CoA:acetate CoA transferase (*but* gene) or by butyrate kinase (*buk* gene) after phosphorylation of butyryl-CoA, generating acetyl-CoA as well (Saint-Amans et al., 2001; Vital et al., 2014).

Certain bacterial strains of *Eubacterium hallii* and *Anaerostipes caccae*, known for their ability to produce butyrate, were also found to metabolize both isomers of LA. When cultivated with DL-lactate, these strains utilized the entire substrate and converted it to butyrate at concentrations exceeding 20 mM. The proposed metabolic pathway for this conversion involves the acetyl-CoA pathway, following the conversion of LA

to pyruvate and subsequently to acetyl-CoA by the enzymes LDH and pyruvate dehydrogenase (PDH), respectively. When *E. hallii* and *A. caccae* strains were provided with a complex substrate derived from starch biodegradation containing both lactate and acetate, they converted the full amount of LA and approximately half of the acetate to butyrate, as indicated by the molar ratio of substrates to butyrate (Duncan et al., 2004).

**3.4.2.2. Caproic acid.** The bioproduction of caproic acid (CA) involves a well-known chain elongation process that extends from acetate (two-carbon molecule) to butyrate (four-carbon molecule), and subsequently to caproate (six-carbon molecule) through the reverse  $\beta$ -oxidation pathway. While the conversion from acetate to butyrate is well understood, the key enzymes responsible for synthesizing caproyl-CoA and CA remain largely unidentified (Fig. 3, Pathway D). It is assumed that the enzymes involved in butyrate synthesis via reverse  $\beta$ -oxidation also play a role in the formation of CA, although this is not always supported by physiological and genomic studies (Lu et al., 2021).

Microbial CA production requires synthesis of acetyl-CoA and butyryl-CoA prior to CA formation. In the case of LA being the carbon source, the former is, presumably, established via LA oxidation to pyruvate and subsequently to acetate, generating acetyl-CoA. Additionally, LA oxidation would provide the necessary acetyl-CoA for the acetate to elongate its carbon length to form butyrate, according to the pathway described above. Subsequently, another acetyl-CoA molecule derived from LA would enter the cycle of reverse  $\beta$ -oxidation to form the key intermediate caproyl-CoA via four consecutive enzymatic steps. Finally, condensation of either caproyl-CoA and acetate or caproyl-CoA and butyrate yields CA (Lu et al., 2021; Zhu et al., 2015).

So far, a couple of native microbial systems have been studied for their CA production potential with LA as the sole carbon source. Among the studied strains, *Megasphaera hexanoica* demonstrated the highest efficiency and productivity with a yield of 0.9 g CA/g substrate (Kang et al., 2022), followed by *Ruminococcaceae bacterium* CPB6 with 0.3 g/g (Zhu et al., 2017), and *Megasphaera elsdenii* J1 with 0.1 g/g (h) (Marounek et al., 1989). In more detail, *M. hexanoica* produced 8.9 g/L CA from 10 g/L LA and compared to fructose, that is the conventional substrate for CA production by *M. hexanoica*, LA resulted in 4-fold less biomass. However, it generated 3-fold more CA, ultimately leading to similar final CA titers, demonstrating the higher specific productivity of LA compared to fructose. Conversely, *R. bacterium* CPB6 growing on LA displayed minimal differences in cell growth profiles compared to glucose, but exhibited earlier initiation of CA production, resulting in higher final titers and productivity.

## 3.5. 1,4-Butanediol

### 3.5.1. 4-Hydroxybutyric acid and the TCA cycle

Non-pathogenic pseudomonads, especially *P. putida* strains, have emerged as valuable model organisms in bioremediation, biodegradation, and bio-upcycling, owing to their exceptional metabolic versatility and adaptability to diverse physicochemical and nutritional conditions. These Gram-negative,  $\gamma$ -Proteobacteria are resilient to environmental stresses and produce various bioactive compounds. Notably, *P. putida* can accumulate intracellular polyester granules, i.e., PHAs, in response to carbon excess, offering potential as a substitute for conventional plastics.

Particularly, *P. putida* KT2440 is a well-characterized strain that excels as a synthetic biology chassis due to its genetic modifiability, rapid growth rate, and low nutrient demand. Moreover, it exhibits remarkable metabolic versatility towards a variety of carbon sources, including alcohols and aldehydes, and extensive genome-scale modelling studies have enabled the understanding of its intracellular metabolic mechanisms that proceed via a broad spectrum of native oxygenases, oxidoreductases, hydrolases, transferases and

dehydrogenases (Nelson et al., 2002; Nikel et al., 2014; Nikel and de Lorenzo, 2018).

The working mechanism for BDO degradation (Fig. 3) involves a two-step conversion of BDO to 4HB via 4HB-aldehyde, with the sequential catalytic action of an aldehyde dehydrogenase and an alcohol dehydrogenase. At the point of 4HB, two putative pathways are branching off. According to the direct oxidation pathway (Fig. 3, Pathway E), 4HB is first oxidized to succinate semialdehyde and eventually to succinate, which then enters the TCA cycle. WT *P. putida* KT2440 can grow on BDO as the sole carbon source, albeit with slow rates. Although proteomics data have confirmed the presence of relevant oxidoreductases that could catalyze BDO direct oxidation, it appears that in WT *P. putida* the bottleneck of this pathway is the oxidation of 4HB to succinate, indicated by the accumulation of 4HB in BDO-fed cultures (Li et al., 2020).

According to the alternative  $\beta$ -oxidation pathway (Fig. 3, Pathway F), 4HB is CoA-activated via CoA ligases or transferases and undergoes  $\beta$ -oxidation that would result in acetyl-CoA and glycolyl-CoA (Li et al., 2020). The former directly enters the TCA cycle, while glycolyl-CoA may be converted to glycolate and subsequently to glyoxylate. Glyoxylate, then, would either follow the glyoxylate shunt, leading to the production of malate or isocitrate that could enter the TCA cycle, or would be directed to the gcl pathway (Section 3.3.1.1). The gcl pathway results in the formation of glycerate, which is eventually phosphorylated to either of two glycolytic intermediates, glycerate 3-phosphate or glycerate-2-phosphate (Clark and Cronan, 2005).

ALE, atmospheric pressure room temperature plasma induced mutation, and genetic engineering—either for gene knockouts or insertions—have been employed towards the enhancement of *P. putida* KT2440 growth on BDO. Genome sequencing, transcriptomics, and proteomics have shed light on the molecular mechanisms underlying BDO degradation and utilization. ALE studies managed to obtain two evolved strains with 4-fold improved growth rates on BDO and lower 4HB accumulation. Based on knockout analyses and reverse-engineering, additionally supported by associated proteomics data, it was suggested that the evolved strains mainly proceed through the direct oxidation pathway towards SA, although the alternative  $\beta$ -oxidation hypothesis is possibly also operative (Li et al., 2020).

Atmospheric and room-temperature plasma combined with ALE resulted in the mutant *P. putida* NB10 that exhibited a 5-fold higher growth performance on BDO compared to the parental strain, and better tolerance against aldehydes that are putative metabolic intermediates of BDO degradation. Transcriptomics on *P. putida* NB10 revealed that TCA-related genes were downregulated compared to the KT2440 strain, while transcription of genes in the gcl pathway was upregulated, and the mutated gcl cluster promotor was shown to confer 17–74 times higher transcription. Based on the above, the authors suggested that BDO metabolism in NB10 strain, certainly proceeds via the alternative  $\beta$ -oxidation/gcl pathway (Qian et al., 2023).

*P. putida* KT2440 is one of the few microorganisms that possess both the metabolic pathways for 4HB biosynthesis and PHAs production, making it an excellent candidate for the biosynthesis of the valuable homopolymer P4HB. When two *P. putida* KT2440 evolved strains were grown under nitrogen limitation with BDO and octanoic acid as co-substrates (4:1 ratio), P4HB yields were about 60 %. When BDO was the sole carbon source though, both strains performed poorly, if at all (Li et al., 2020). *P. putida* NB10 on the other hand, accumulated 50 % more P4HB compared to the parental KT2440 strain when grown solely on BDO, while transcription of key genes associated with P4HB synthesis was upregulated (Qian et al., 2023). P4HB homopolymer synthesis is, presumably, enhanced via an interruption of the TCA cycle and redirection of the carbon flux towards the 4HB shunt, that would result in CoA-activation of 4HB and eventual synthesis of P4HB by PhaC (Utsunomia et al., 2020). This hypothesis is further supported by an unrelated study on an engineered *E. coli* strain, where deletion of succinate semialdehyde dehydrogenase genes eliminated succinate

formation and led to increased 4HB synthesis (Li et al., 2010). Similarly, in *P. putida* and *Pseudomonas entomophila*, inhibition of  $\beta$ -oxidation via gene deletion has been shown to redirect the metabolic flux from fatty acid degradation to PHA biosynthesis, hence, significantly increasing substrate conversion efficiency and PHA synthesis (Chen and Jiang, 2017).

Besides Pseudomonads, *G. oxydans* DSM50049 can also utilize BDO as a carbon source (Ismail et al., 2024). Its genome reveals an incomplete TCA cycle, lacking genes for succinate dehydrogenase and succinyl CoA synthetase, leading to a unique strategy of incomplete oxidation. This allows *G. oxydans* to thrive in nutrient-rich environments despite low energy efficiency and growth yields (Prust et al., 2005). BDO catabolism in *G. oxydans* proceeds through the direct oxidation pathway, as in *P. putida* KT2440. Depending on the culture pH, *G. oxydans* produces either 4HB or a mix of 4HB and SA, with complete substrate consumption in both cases. At neutral pH, only 4HB is produced with an 88 % yield, while at pH 5.0, both products are in equal molar ratios, indicating pH sensitivity of 4HB dehydrogenase and succinate semialdehyde dehydrogenase.

### 3.5.2. Malic acid

MLA is naturally synthesized in all organisms during cellular metabolism, but its accumulation is only associated with stress conditions or mutant strains. Due to its high commercial value, diverse applicability, and the relatively expensive industrial production routes, microbial production of MLA has attracted research interest. Apart from being cost efficient, microbially produced MLA is also advantageous due to its optically pure L-form as opposed to racemic mixtures produced by chemical processes (Khandelwal et al., 2023). Since its first identification as a yeast fermentation product in the early 20th century (Dakin, 1924), various native fungal species have been used as natural MLA producers, and genetic and metabolic engineering approaches have been employed for the optimization of the process. So far, three different native cellular pathways are known to lead to MLA synthesis (Fig. 3), and these have also been the focus of engineering attempts. The oxidative TCA cycle starts with the synthesis of citric acid followed by several oxidative reactions to synthesize MLA, while the reductive TCA pathway leads to MLA via a two-step enzymatic conversion of pyruvate. MLA is also synthesized through the gcl pathway which acts as an anaplerotic intracellular mechanism.

In the frame of plastic waste streams valorization, a recent study screening native *Ustilaginaceae* strains capable of producing MLA identified *Ustilago trichophora* TZ1 as the first fungal strain that could grow on BDO as the sole carbon source (Phan et al., 2024). Interestingly, this strain would produce MLA and SA while grown on glycerol (Zambanini et al., 2016), but when BDO was used as carbon source, the polyols mannitol and erythritol were additionally produced (Phan et al., 2023). ALE combined with culture optimizations, enhanced growth of *U. trichophora* TZ1 on BDO, with MLA yields reaching 33 % (Phan et al., 2023). The concomitant production of sugar alcohols has not been studied further, but the pathway that could be envisaged proceeds via the 4HB intermediate, the TCA cycle, pyruvate generation, and gluconeogenesis that results in the production of Glu-6-P. The latter is the precursor for the biosynthesis of both mannitol and erythritol, that are produced via established intracellular pathways (Nakagawa et al., 2020; Wisselink et al., 2002).

### 3.5.3. Rhamnolipids synthesis

Rhamnolipid synthesis relies on two widely known pathways, i.e., fatty acid de novo synthesis and the rhamnose pathway, providing the required precursors 3-(3-hydroxyalkanoyloxy) alkanolic acid and activated deoxy-thymidine-diphospho-L-rhamnose (dTDP-L-rhamnose), respectively (Fig. 3, Pathway G). Unlike molecules synthesized through a single pathway, rhamnolipids synthesis requires two central carbon metabolism intermediates: acetyl-CoA for 3-(3-hydroxyalkanoyloxy) alkanolic acid and Glu-6-P—the first intermediate of glucose



metabolism—for dTDP-L-rhamnose. In the rhamnose pathway, Glu-6-P is initially converted to Glu-1-P by an enzyme with phosphoglucotransferase activity. Glu-1-P is then transformed into rhamnose by the concerted action of four enzymes, a G1P thymidyltransferase (RmlA), a dTDP-D-glucose 4,6-dehydratase (RmlB), a dTDP-6-deoxy-D-xylo-4-hexulose 3,5-epimerase (RmlC), and a dTDP-6-deoxy-L-lyxo-4-hexulose reductase (RmlD) (Giraud and Naismith, 2000; Maier and Soberón-Chávez, 2000).

*Pseudomonas aeruginosa* possesses the essential genes for rhamnolipid synthesis, which involves three dedicated enzymatic reactions. Initially, RhlA, a 3-hydroxyacyl-ACP-O-3 hydroxyacyltransferase, catalyzes the dimerization of 3-hydroxyacyl-ACP, descending from the fatty acid de novo synthesis, forming 3-(3-hydroxyalkanoyloxy) alkanolic acid. Subsequently, RhlB, a rhamnosyltransferase I, condenses 3-(3-hydroxyalkanoyloxy) alkanolic acid with dTDP-L-rhamnose to produce mono-rhamnolipids. The final step involves RhlC, a rhamnosyltransferase II, which adds another rhamnose moiety to the mono-rhamnolipid, resulting in a di-rhamnolipid. The genes *rhlA* and *rhlB* are organized in a single operon, whereas *rhlC* is located elsewhere in the *P. aeruginosa* genome, forming an operon with a gene of unknown function (Tiso et al., 2016; Wittgens et al., 2017).

As mentioned previously, *P. putida* KT2440 was submitted to ALE to be able to metabolize BDO (Li et al., 2020). Afterwards, the evolved strain was engineered with the *rhlAB* operon from *P. aeruginosa* to facilitate mono-rhamnolipid production and it was, indeed, shown to produce 0.13 g/L mono-rhamnolipids, with a yield of 0.09 g/g of substrate (Utomo et al., 2020). Although the metabolic processes underlying BDO upcycling to mono-rhamnolipids were not studied in detail, one could picture a scenario where BDO is intracellularly catabolized via the discussed pathways, eventually reaching the level of G6P and, additionally, fueling de novo fatty acid synthesis.

### 3.6. Succinic acid

#### 3.6.1. BDO formation

Intracellularly, SA is first activated by succinyl-CoA synthetase (SucCD), and is, subsequently, converted to succinate semialdehyde by a CoA-dependent succinate semialdehyde dehydrogenase (SucD). 4HB dehydrogenase (4HBd) catalyzes 4HB formation, that can be activated by 4HB-CoA transferase (Cat2). From that point, two consecutive reductive steps, catalyzed by 4HB-CoA reductase and aldehyde dehydrogenase, can lead to the formation of 4HB-aldehyde and BDO, respectively (Fig. 3) (Burk et al., 2015; Yim et al., 2011).

*E. coli* naturally catalyzes the conversions of SA to succinyl-CoA and 4HB-aldehyde to BDO. An engineered *E. coli* system, with heterologous gene expression accounting for the missing steps, was shown to convert SA all the way to BDO (Yim et al., 2011). Specifically, the enzyme SucD from *Porphyromonas gingivalis* was found to be critical for 4HB production, while co-expression of a 4HB dehydrogenase from the same microorganism further enhanced 4HB yield. By constructing a synthetic operon that sequentially incorporates *sucCD* from *E. coli*, and *sucD* and 4HBd from *P. gingivalis*, a significantly higher 4HB:SA ratio was achieved. Additionally, the expression of the aldehyde/alcohol dehydrogenase adhE2, responsible for the conversion of 4HB-aldehyde to BDO, from WT *C. acetobutylicum*, alongside the expression of the *cat2* gene from *P. gingivalis*, were optimized for use in *E. coli*, to facilitate BDO production.

#### 3.6.2. PHAs synthesis

Various WT bacterial strains exhibit the capacity to utilize SA and synthesize PHAs, although the exact molecular mechanism is not definitive. Based on the available knowledge, it is likely that this conversion proceeds via the conversion of SA to acetyl-CoA through the TCA cycle, followed by the subsequent synthesis of PHAs through the established bacterial pathways (Pradhan et al., 2020). For instance, when supplied with SA as the sole carbon source, *R. palustris* SP5212 was

able to accumulate PHAs, with P3HB accounting for approximately 3 % CDW (Mukhopadhyay et al., 2005). Bacterial strains *C. glutamicum* DSM 20137 and *Bacillus megaterium* DSM 509, on the other hand, synthesized pure P3HB, representing 10 % and 45 % CDW, respectively. *P. putida* mt-2 accumulated mcl-PHAs at about 15 % CDW, with the C<sub>10</sub> monomer (3-hydroxydecanoate) comprising 60 % of the total PHAs produced (Shahid et al., 2013).

### 3.7. Adipic acid

Microbial assimilation of AA by *Acinetobacter baylyi* is encoded in two separate operons and depends on the concerted action of dedicated transporters and enzymes (Fig. 2, Pathway G). One operon encodes the transport proteins DcaK and DcaP, the CoA transferase subunits DcaIJ, and the acyl-CoA dehydrogenase DcaA, whose concerted action results in the production of 2,3-didehydro-adipyl-CoA. The latter is further degraded to acetyl-CoA and succinyl-CoA via  $\beta$ -oxidation, which depends on the *dcaECHF* operon that includes an enoyl-CoA hydratase (DcaE), a hydroxyacyl-CoA dehydrogenase (DcaH), and an acyl-CoA thiolase (DcaF) (Ackermann et al., 2021).

#### 3.7.1. PHAs synthesis

Building upon the inherent capacity of *P. putida* KT2440 to synthesize PHAs from diverse carbon substrates (Liu et al., 2022a), metabolic engineering efforts targeted the expression of the *dcaAKIJP* operon, complemented by the organism's innate genetic repertoire for the downstream metabolic pathway, i.e.,  $\beta$ -oxidation. Unexpectedly, the engineered strain could not grow on AA as the sole carbon source, but subsequent ALE supported growth as well as PHAs production with a yield of about 25 % CDW, leading to the hypothesis that the native *P. putida* genes for  $\beta$ -oxidation were not induced previously. The PHAs produced were composed of C<sub>6</sub>, C<sub>8</sub>, C<sub>10</sub>, and C<sub>12</sub> monomers, with the C<sub>10</sub> being the more predominant, accounting for 56 % of the total (Ackermann et al., 2021).

Sullivan and coworkers (Sullivan et al., 2022) studied the valorization of mixed plastics starting with metal-catalyzed autooxidation of different combinations of polystyrene, high-density polyethylene, and PET mixtures, that yielded oxygenated small organic molecules. Their microbial upcycling approach was focused on the production of  $\beta$ KA and PHAs, demonstrating a tunable bioconversion microbial chassis. The authors based their metabolic design on two previously engineered *P. putida* strains from (Werner et al., 2021) (Section 3.2.3) and (Ackermann et al., 2021) (current Section). In summary, the new *P. putida* AW162 strain was capable of: (i) TPA assimilation and conversion to PCA (engineered pathway), (ii) PCA 3,4-cleavage pathway (native pathway) leading to the TCA cycle (Section 3.2.3 & Fig. 2, Pathway C), (iii) AA assimilation due to the incorporation of the *A. baylyi dca* gene cluster (engineered pathway), along with the deletion of native *paaX* and *psrA*, which repress phenylacetate catabolism and  $\beta$ -oxidation, respectively, and (iv) PHAs production (native pathway). Indeed, *P. putida* AW162 could produce mcl-PHAs, primarily comprised of C<sub>10</sub> and C<sub>12</sub>, when grown on effluent from mixed postconsumer high-density polyethylene bottles and expanded polystyrene cups. *P. putida* AW307 was tuned towards  $\beta$ KA accumulation instead, and thus its native PCA 3,4-cleavage pathway was interrupted by the *pcaIJ* gene deletion. *P. putida* AW307 grew on a model mixture and an effluent of the depolymerized mixed plastics—both containing benzoate, terephthalate, C<sub>4</sub>-C<sub>18</sub> dicarboxylates, and acetate—and  $\beta$ KA was produced at a 76 % molar yield (calculated on benzoate and terephthalate) (Sullivan et al., 2022).

#### 3.7.2. 1,6-diaminohexane synthesis

The microbial conversion of AA to DAH is another upcycling system that has been constructed, based on the action of select CARs and transaminases (TA). According to the simplest pathway, AA is first reduced to adipic semialdehyde, which is, subsequently, converted into



either adipaldehyde or 6-aminocaproic acid. Both these intermediates are then metabolically transformed into 6-aminohexanoic acid, which is further transaminated to DAH (Fig. 2, Pathway H).

An *E. coli* BL21 strain was selected for the construction of a whole-cell artificial pathway for DAH biosynthesis, due to its inherent tolerance to DAH and its intermediate, 6-aminocaproic acid. In the first step, the strain was genetically engineered to heterologously express genes encoding a CAR from *Mycobacteroides abscessus* (MAB CAR), a TA from *Chromobacterium violaceum* (CVTA) and a phosphopantetheinyl transferase (SFP) from *B. subtilis* (Quadri et al., 1998). The necessity of enzymes with these functionalities for the conversion of AA to DAH was validated, and various CAR and TA enzymes from diverse microbial sources were evaluated, both individually and in combinations. The selection and arrangement of different CARs and TAs in the constructed vectors influenced the efficiency of reduction and transamination for the intermediate conversions. The most efficient cascade module for DAH synthesis was found to be the CAR – CAR – TA – TA (CCTT) branch, that was comprised of a CAR from *Mycobacterium smegmatis* MC2 I55 (MSM CAR), a MAB CAR, a TA from *Silicibacter pomeroyi* (SPTA), and a TA from *E. coli* (PatA); the latter was proven to be essential for 6-aminohexanoic acid transamination to DAH. Furthermore, given that CARs are NADPH-dependent enzymes, optimization of NADPH supply to the system was crucial. Indeed, the deletion of the *sthA* gene, encoding a transhydrogenase isoenzyme responsible for the mutual transformation between NADH and NADP in *E. coli*, resulted in a significant enhancement of DAH yield. In the end, the engineered *E. coli* strain achieved a production of 239 mg/L of DAH in shake flask fermentation, more than 500-fold increase relative to the initial strain (Wang et al., 2023).

### 3.8. 6-hydroxyhexanoic acid

#### 3.8.1. Adipic acid production

The metabolic pathway of cyclohexanol utilization by *Acinetobacter* has been elucidated already for 50 years and is known to depend on at least five enzymes that work consecutively to produce AA (Iwaki et al., 1999). In this pathway, HHA serves as the third metabolic intermediate that is converted to 6-oxohexanoic acid by HHA dehydrogenase (*chnD*), and eventually to AA by the action of 6-oxohexanoate dehydrogenase (*chnE*) (Fig. 2). Two recent independent studies managed to engineer *E. coli* JM109 to express the gene products of *chnE* and *chnD* and, therefore, yield about 2–4 g/L AA when HHA was supplied in batch fermentations. By regulating the addition of HHA during fed-batch fermentations, AA production increased approximately 3.6-fold, reaching about 16 g/L (Oh et al., 2022, 2023).

## 4. Significance and applications of added-value products

### 4.1. Aromatics

Aromatic compounds, particularly phenolic acids and derivatives, possess a variety of biological and industrial applications. These compounds exhibit significant antioxidant, anti-inflammatory, antimicrobial, and anticancer properties, along with diverse uses in pharmaceuticals, food preservation, and material science.

Protocatechuic acid (PCA; IUPAC: 3,4-dihydroxybenzoic acid) is a potent antioxidant with anti-inflammatory, antihyperglycemic, anticancer, and antimicrobial properties. It mitigates oxidative stress by scavenging free radicals, reduces reactive oxygen species, and boosts endogenous antioxidant enzymes, protecting against degenerative diseases. PCA also regulates inflammatory mediators, improves glucose homeostasis, and promotes apoptosis in cancer cells. Its diverse therapeutic applications include antiulcer, antiaging, antifibrotic, cardioprotective, and neuroprotective effects, with potential in preventing colon cancer, managing type 2 diabetes, and protecting against toxicity from both natural and synthetic agents (Kakkar and Bais, 2014; Kelidari et al., 2024). Its antimicrobial effects against various bacteria and fungi

suggest applications in health protection and food preservation (Semaming et al., 2015).

Gallic acid (GA; IUPAC: 3,4,5-trihydroxybenzoic acid) is known for its antioxidant, anti-inflammatory, and neuroprotective properties, especially in the treatment of neurodegenerative diseases like Alzheimer's and Parkinson's. It acts through modulation of oxidative stress and inflammation, with applications in managing psychiatric disorders and neuroinflammation. GA also has anticancer potential due to its prooxidant activity, inducing apoptosis in cancer cells (Bhuia et al., 2023; Kahkeshani et al., 2019). Beyond health applications, it is widely used in food preservation, cosmetics, and leather tanning (Badhani et al., 2015).

Catechol (IUPAC: benzene-1,2-diol) is a versatile compound found in fruits, vegetables, and as a metabolic product in humans (Schweigert et al., 2001). It serves as an intermediate in various industrial processes, including the production of antioxidants, polymers, and in the cosmetic and pharmaceutical industries, in photographic development and as a flavoring agent (National Center for Biotechnology Information, 2024a). Catechol's unique adhesive properties, inspired by mussel proteins, are also being explored for synthetic coatings and biomedical materials (Zhang et al., 2022).

Pyrogallol (PG; IUPAC: benzene-1,2,3-triol) is a trihydroxybenzene with strong reducing and antioxidant properties. Historically used in photographic development, PG has applications in dyeing, environmental monitoring, medicinal chemistry, and materials science (National Center for Biotechnology Information, 2024b). It also plays a role in the preparation of metal colloids and as an analytical reagent for oxygen measurement. Its natural occurrence in hardwoods like oak and eucalyptus highlights its longstanding relevance in both traditional and modern uses.

Vanillic acid (VA; IUPAC: 4-hydroxy-3-methoxybenzoic acid) is a phenolic compound found in medicinal plants and used as a flavoring agent (National Center for Biotechnology Information, 2024c). VA demonstrates anticancer, anti-obesogenic, antidiabetic, and antimicrobial effects. It induces apoptosis, inhibits cancer cell cycle progression, and mitigates oxidative stress and inflammation (Kaur et al., 2022). VA also holds potential in treating obesity and metabolic disorders, as well as offering cardioprotective and hepatoprotective benefits (Ingole et al., 2021).

Vanillin (IUPAC: 4-hydroxy-3-methoxybenzaldehyde), the primary compound in vanilla extract, is widely used as a flavoring agent but also exhibits antioxidant, anti-inflammatory, anticancer, and antidiabetic properties. While often considered merely a food additive, research indicates that vanillin has significant therapeutic potential, warranting further exploration for clinical applications due to its bioavailability (Olatunde et al., 2022).

2-Pyrone-4,6-dicarboxylic Acid (PDC; IUPAC: 2-oxo-2H-pyran-4,6-dicarboxylic acid) is a pseudoaromatic compound obtained through microbial conversion of PCA (Kang et al., 2020). Its structure enables polymerization with diols to form biodegradable polyesters with enhanced mechanical properties. PDC-based polyesters, polyamides, and polyurethanes exhibit excellent biodegradability, thermal stability, and elasticity, making them valuable in producing eco-friendly materials (Otsuka et al., 2023; Zhou et al., 2023c).

L-tyrosine (IUPAC: (2S)-2-amino-3-(4-hydroxyphenyl)propanoic acid) is a non-essential amino acid with diverse applications, synthesized in vivo from L-phenylalanine. It serves as a precursor for catecholamines such as dopamine, norepinephrine, and epinephrine, as well as thyroid hormones and melanin, emphasizing its critical role in neurological and metabolic functions. In the brain, dietary tyrosine directly influences neurotransmitter levels, which are vital for stress response and cognitive performance. Beyond its biological significance, L-tyrosine is utilized as a flavoring agent, nutritional supplement, and ingredient in hair and skin conditioning products in the cosmetics industry. Its applications in treating phenylketonuria, biochemical depression, and Parkinson's disease highlight its therapeutic potential,

although certain claims remain inconclusive (National Center for Biotechnology Information, 2025a).

Phenylalanine (IUPAC: (2S)-2-amino-3-phenylpropanoic acid) is an essential aromatic amino acid fundamental to protein biosynthesis and a precursor to tyrosine. It plays a pivotal role in the production of catecholamines, including dopamine and norepinephrine, which are integral to the nervous system (National Center for Biotechnology Information, 2025b). L-phenylalanine is also a key component in artificial sweeteners like aspartame, underscoring its industrial importance (Doble and Kruithventi, 2007). Beyond food applications, its therapeutic uses extend to managing vitiligo, chronic pain, and certain mood disorders (National Center for Biotechnology Information, 2025b).

p-Coumaric acid (IUPAC: (E)-3-(4-hydroxyphenyl)prop-2-enoic acid) is a naturally occurring phenolic compound found in a variety of vegetables and fruits. Known for its antioxidative properties, it mitigates oxidative stress, reducing the risk of cardiovascular diseases (Ponnian et al., 2024). p-Coumaric acid also has applications in cosmetics as a skin-conditioning agent, while its potential in food preservation leverages its antimicrobial effects (National Center for Biotechnology Information, 2025c). Additionally, its role as a precursor in synthesizing bio-based and biodegradable materials supports the development of sustainable industrial solutions (Singh et al., 2020; Zhang et al., 2025).

#### 4.2. Saturated monocarboxylic acids

Saturated monocarboxylic acids are widely used in various industries and have significant biological effects. These compounds, ranging from small alpha-hydroxy acids to fatty acids, play crucial roles in therapeutic applications, skincare, flavoring, and industrial processes.

Glycolic acid (IUPAC: 2-hydroxyacetic acid) is the smallest alpha-hydroxy acid and is extensively used in dermatology, particularly for chemical peels. It addresses skin concerns like wrinkles, acne scarring, and hyperpigmentation by facilitating exfoliation and revealing fresher skin. As a keratolytic agent, it also aids in treating corns, warts, and fungal infections (Chemical Entities of Biological Interest (ChEBI), 2021). Beyond skincare, glycolic acid is used in food processing, textile and leather dyeing, metal processing, adhesives manufacturing, and ink production, improving flow properties and gloss (National Center for Biotechnology Information, 2024d).

2,4-dihydroxybutyric acid (DHB; IUPAC: 2,4-dihydroxybutanoic acid) is a hydroxy-substituted short-chain fatty acid derived from butyric acid (National Center for Biotechnology Information, 2025d). Its industrial relevance stems from its role as a versatile platform molecule for synthesizing value-added products. It serves as an intermediate in producing 1,3-propanediol and 1,2,4-butanetriol—key compounds in the manufacturing of plastics, solvents, and propellants. Under acidic conditions, 2,4-dihydroxybutyric acid spontaneously forms 2-hydroxy- $\gamma$ -butyrolactone, which can be further processed into  $\gamma$ -butyrolactone and 1,4-butanediol, both critical in polymer production. Additionally, it contributes to the synthesis of the methionine analog 2-hydroxy-4-(methylthio)butyrate, widely utilized in animal nutrition (Walther et al., 2017).

Butyric acid (IUPAC: butanoic acid) is a short-chain fatty acid with significant therapeutic potential. It exhibits anti-inflammatory and anticancer properties by modulating transcription factors involved in immune response. Butyrate, its active form, is beneficial for managing gastrointestinal disorders such as irritable bowel syndrome and Crohn's disease by enhancing intestinal barrier function. Butyrate also influences the gut-brain axis, affecting metabolism and systemic functions, and is useful in treating skin conditions like atopic dermatitis and psoriasis (Liu et al., 2018) (Coppola et al., 2022).

Caproic acid (CA; IUPAC: hexanoic acid) is a six-carbon chain fatty acid synthesized endogenously and found in plants. It serves as a precursor in producing esters used in perfumery, pharmaceuticals, and the polymer industry. Caproic acid is also a flavoring agent with a distinctive cheesy odor and is utilized in making metal hexanoates for use as

drying agents in paints and varnishes (National Center for Biotechnology Information, 2024e).

4-Hydroxybutyric acid (4HB; IUPAC: 4-hydroxybutanoic acid), also known as  $\gamma$ -hydroxybutyric acid, is derived from butyric acid and acts as a neurotransmitter. It is used in medical applications, such as a general anesthetic and to treat narcolepsy-related conditions. 4HB influences neurotransmitter activities by crossing the blood-brain barrier and interacting with specific receptors, leading to central nervous system depression (Chemical Entities of Biological Interest (ChEBI), 2024; National Center for Biotechnology Information, 2024f).

#### 4.3. Saturated dicarboxylic acids

Saturated dicarboxylic acids, including adipic acid and succinic acid, are key intermediates in industrial processes and have a wide range of applications across multiple sectors, such as polymers, food, pharmaceuticals, and environmental management.

Adipic acid (AA; IUPAC: hexanedioic acid) is a key aliphatic  $\alpha,\omega$ -dicarboxylic acid and a primary precursor for nylon-6,6 production, which accounts for around 90 % of its use. It is also used in manufacturing polyester polyols for polyurethane systems (National Center for Biotechnology Information, 2024g). In addition to its role in polymers, AA is employed in producing plasticizers, lubricants, and food additives (E355), such as gelling agents, acidulants, and leavening agents. It is further utilized in pesticides, dyes, textile treatments, fungicides, and pharmaceuticals (Goldberg and Rokem, 2009). However, its production can release  $N_2O$ , a potent greenhouse gas, prompting efforts to reduce emissions from production facilities (Shimizu et al., 2000).

Succinic acid (SA; IUPAC: butanedioic acid) is a valuable four-carbon dicarboxylic acid with applications in food, cosmetics, and chemistry. As an intermediate in the TCA cycle, SA contributes to cellular energy production and serves as a precursor for many compounds (National Center for Biotechnology Information, 2024h). In the food industry, it functions as a flavor enhancer and acidity regulator (E363). It is also used in detergents, cosmetics, dyes, and pharmaceuticals, particularly in treatments for metabolic diseases and diabetes (Lee et al., 2019). Additionally, SA has antibiotic properties and can support neural recovery and immune function. It is a precursor for chemicals like BDO,  $\gamma$ -butyrolactone, and tetrahydrofuran, as well as bio-based polymers like PBS and PBSA. Moreover, SA and its derivatives are employed in the leather and metallurgy industries for water resistance, strength enhancement, and ore flotation (Raj et al., 2024).

#### 4.4. Unsaturated dicarboxylic acids

Unsaturated dicarboxylic acids, including muconic acid,  $\beta$ -keto-adipic acid, and malic acid, are essential compounds with significant roles in industrial and biological applications. These acids contribute to various processes in polymer chemistry, bioplastics, food, and pharmaceuticals, while also offering sustainable alternatives to traditional materials.

Muconic acid (MA; IUPAC: (2E,4E)-hexa-2,4-dienedioic acid) is a conjugated dicarboxylic acid derived mainly from the oxidative cleavage of benzene derivatives. It serves as a critical precursor for producing high-demand chemicals like AA and TPA, essential in nylon, polyurethanes, and polyesters (Khalil et al., 2020). MA exists in three isomeric forms—*cis,cis*-MA, *cis,trans*-MA, and *trans,trans*-MA—each with distinct chemical properties for diverse applications. In addition to polymer chemistry, MA is used in bioplastics, functional resins, agrochemicals, and as an intermediate in food additives, medicines, cosmetics, and textiles (Choi et al., 2020; Wang et al., 2020a).

$\beta$ -keto-adipate ( $\beta$ KA; IUPAC: 3-oxohexanedioic acid) is a six-carbon diacid that serves as an alternative to AA in nylon-6,6 analogue production. Featuring a  $\beta$ -ketone group,  $\beta$ KA results in materials with improved thermal stability and reduced water permeability. Biologically synthesized from sugars,  $\beta$ KA offers a sustainable alternative to fossil-

based AA, requiring significantly less energy and generating fewer greenhouse gases. The same bioprocess also yields products with superior performance characteristics, making it an environmentally friendly choice for bio-based polymer production (Rorrer et al., 2022).

Malic acid (MLA; IUPAC: 2-hydroxybutanedioic acid) is an alpha-hydroxy acid naturally found in fruits and wines, with multiple roles in food and biological systems. It serves as a food acidity regulator and enhances flavors in beverages, jams, and candies. In skincare, MLA helps exfoliate dead skin cells and stimulates saliva production for individuals with dry mouth. As a key metabolite in the Krebs cycle, it plays a critical role in energy production (National Center for Biotechnology Information, 2024i). Additionally, MLA is used in metal cleaning, textile finishing, water treatment, and fabric dyeing. Its biopolymer, poly( $\beta$ -L-MLA), is biocompatible, biodegradable, and water-soluble, making it ideal for drug delivery systems and advanced biomaterials (Lee et al., 2019).

#### 4.5. Saturated and functionalized organic compounds

Saturated and functionalized organic compounds, such as BDO and DAH, play crucial roles in various industries, from pharmaceuticals and polymers to sustainable material development. Their versatility as intermediate compounds and their use in producing high-performance materials make them essential to modern manufacturing processes.

1,4-butanediol (BDO; IUPAC: butane-1,4-diol) is a straight-chain glycol with hydroxyl groups at both ends, renowned for its versatility as an intermediate compound. BDO is utilized across several industries, including pharmaceuticals, food, cosmetics, and plasticizers. It serves as a humectant, solvent, food additive, and pharmaceutical intermediate. BDO is also used in the production of polyurethane elastomers, contributing to automotive parts, footwear, and recreational equipment. Furthermore, it is integral to the synthesis of tetrahydrofuran and  $\gamma$ -butyrolactone, essential in electronics, pharmaceuticals, and agrochemicals (National Center for Biotechnology Information, 2024j). One of BDO's key applications is in the creation of biodegradable polymers such as PBS, PBSA, and PBAT, which are vital for sustainable material development.

1,6-diaminohexane (DAH; IUPAC: hexane-1,6-diamine) is a versatile organic compound, particularly important in polymer synthesis. Its two functional amine groups make it ideal for creating robust and resilient polymers. DAH plays a pivotal role in the production of nylon-6,6, where it reacts with AA in condensation polymerization. This process is critical for manufacturing nylon, which is used extensively in textiles and engineering plastics (Palmer, 2003). Additionally, DAH can undergo phosgenation to generate hexamethylene diisocyanate, a precursor for polyurethane manufacturing (Hu et al., 2017). DAH is also utilized as a cross-linking agent in resin systems, including epoxy resins, adhesives, and paper manufacturing (Lainioti et al., 2021).

#### 4.6. Biopolymers

The biopolymers polyhydroxyalkanoates (PHAs) and bacterial nanocellulose (BNC) are biodegradable, biocompatible, and non-toxic materials with a broad range of applications. These sustainable alternatives to conventional plastics are gaining attention across industries like healthcare, agriculture, packaging, and beyond.

In healthcare, PHAs are widely used in drug delivery systems, tissue engineering, and medical devices such as sutures, surgical needles, and bone tissue replacements. Specific PHAs, like poly(3-hydroxybutyrate-co-3-hydroxyvalerate), poly(3-hydroxybutyrate-co-3-hydroxyhexanoate), and poly(3-hydroxybutyrate-co-4-hydroxybutyrate), are employed for skin regeneration, bone tissue engineering, and heart valve replacements, respectively (Pandey et al., 2022). In the packaging industry, PHAs serve as a sustainable alternative to petroleum-based plastics, being used in products such as plastic bags, food packaging, and disposable items like utensils and straws (Ladhari et al., 2023). Furthermore, PHAs are utilized

in agriculture for improving soil structure and water retention, as well as in water treatment processes for denitrification. Additionally, PHAs have potential as biofuels, offering an eco-friendly alternative to traditional fuels (Pandey et al., 2022). The mcl-PHAs P3HB and P4HB are particularly notable for their unique properties and diverse applications, including use in biodegradable polymers and medical devices.

Poly(3-hydroxybutyrate) (P3HB) is widely used in bone tissue engineering, especially in internal bone fixation devices and composite implants, where it supports osteoblast adherence and bone formation. It is also employed in absorbable sutures and wound dressings due to its biocompatibility, tensile strength, and minimal tissue reactivity (Israni and Shivakumar, 2019). Mcl-PHAs like P3HB are also ideal for low mechanical integrity products such as hot melt adhesives, coatings, and as carriers for slow-release bioactives (Muthuraj et al., 2021).

Poly(4-hydroxybutyrate) (P4HB) is a biodegradable thermoplastic polyester known for its strength, elasticity, and biocompatibility. It is widely used in resorbable medical devices, including sutures and surgical meshes, and has been FDA-approved for various medical applications. P4HB's ability to degrade slowly in vivo minimizes complications and enhances long-term mechanical support (Mitra et al., 2021a). Additionally, it is the only type of PHAs that has received FDA approval for medical use, with applications in tissue engineering, drug delivery systems, and even congenital cardiovascular defect repairs (Martin and Williams, 2003; Utsunomia et al., 2020). Despite its high production costs, P4HB represents a significant advancement in medical materials, offering promising applications in tissue engineering and drug delivery (Martin and Williams, 2003; Mitra et al., 2021b).

BNC is a nanomaterial derived from bacterial cellulose, which has exceptional properties, including high porosity, low cytotoxicity, and biocompatibility. BNC emerges as a ribbon-shaped nanomaterial with dimensions typically ranging from 20 to 100 nm in diameter and several  $\mu$ m in length (Kaur et al., 2021). BNC is widely used in biomedical applications as a scaffold for tissue engineering and regenerative medicine. Its three-dimensional network offers substantial mechanical strength, making it ideal for these purposes. Additionally, BNC serves in the food and cosmetics industries as a thickening, stabilizing, and gelling agent (de Amorim et al., 2020). It is also employed in drug delivery systems, enhancing drug stability and facilitating controlled release (Bacakova et al., 2019). BNC has further applications in ion-exchange membranes and fuel cells, contributing to environmentally friendly technologies due to its thermal-oxidative stability (Kaur et al., 2021).

#### 4.7. Lycopene

Lycopene (IUPAC: [6E,8E,10E,12E,14E,16E,18E,20E,22E,24E,26E]-2,6,10,14,19,23,27,31-octamethyldotriaconta-2,6,8,10,12,14,16,18,20,22,24,26,30-tridecaene) is a carotenoid pigment closely related to  $\beta$ -carotene and is responsible for the red colour of various fruits and vegetables, such as tomatoes, pink grapefruits, apricots, and guavas (Mangels et al., 1993). Known for its antioxidant and anti-inflammatory properties, lycopene helps protect cells from oxidative damage caused by environmental toxins and chronic diseases (Javanmardi and Kubota, 2006). A diet rich in lycopene may lower the risk of certain cancers, including prostate and breast cancer (Mazidi et al., 2020), reduce pain, and offer benefits for ocular, neurological, and skeletal health. In addition, lycopene may improve cholesterol levels, potentially reducing the risk of heart disease and premature mortality, as well as enhance the skin's defense against UV-induced damage (Cooperstone et al., 2017; Mozos et al., 2018).

#### 4.8. Rhamnolipids

Rhamnolipids, biosurfactants primarily produced by *Pseudomonas* and *Burkholderia* species, are known for their high surface activity, emulsification, and biodegradability. Their low toxicity and effectiveness in reducing surface and interfacial tension make them valuable in



agriculture, enhanced oil recovery, environmental remediation, food preservation, and pharmaceuticals. In agriculture, rhamnolipids combat plant pathogens and improve soil quality, while in oil recovery, they enhance extraction efficiency. They also aid in hydrocarbon and heavy metal bioremediation, prevent fungal growth in food storage, and show promise in cancer therapy and drug delivery (Thakur et al., 2021; Tiso et al., 2017b). Growing industrial interest is reflected in numerous patents, and in 2024, the first commercial rhamnolipid production plant opened in Slovakia, marking a key step in sustainable biosurfactant manufacturing (Evonik, 2024).

## 5. Concluding remarks

The growing incentive for circular bioplastic economy value chains is reflected by the rising number of scientific studies, global academic and industrial synergies, and expanding funding opportunities, especially the past five years. Polyester upcycling is a promising innovation that adheres to circular economy principles by mitigating global plastic pollution, reducing natural resources depletion, and promoting sustainable industrial practices. Hydrolytic degradation of polymers into oligomers and their constituent building blocks can be followed by microbial assimilation and eventual production of compounds of interest, essentially transforming waste into commercially valuable products.

Among the polyesters examined, PET has received the lion's share of depolymerization and upcycling research, owing to its prevalence in single-use plastics, particularly beverage bottles, food packaging, and disposable containers. In parallel, biodegradable plastics have gained increasing attention for their potential role in circular economy. PLA exemplifies this trend, offering a distinct advantage in that its hydrolysis yields a single monomeric product through de-esterification. Research on sustainable management and upcycling of other polyesters is gaining momentum, as it has become clear that landfilling biodegradable materials alone does not prevent their long-term environmental accumulation. Effective waste management strategies, including industrial composting, controlled (bio)degradation, and upcycling, are essential to facilitate their reintegration into natural biogeochemical cycles or circular value chains.

Successful microbial upcycling designs must meet two conditions, i. e., efficient carbon assimilation from polyester monomers, and functional biosynthetic pathways yielding valuable bioproducts. Thus, bioprospecting and synthetic biology are used in tandem, with the aim of discovering microorganisms naturally capable of performing either and, subsequently, engineering or modifying the other process. Among the several WT microorganisms that have been found capable of either process, *P. putida* is in the limelight, not only due to its central carbon metabolism that supports rerouting of carbon fluxes towards desired inherent pathways via transcription regulation, but also because of its relatively easy genetic manipulation leading to the introduction of novel synthetic pathways. However, many biochemical pathways for plastic degradation and assimilation are found in non-model microorganisms, highlighting the need to explore their metabolic diversity for future advancements in the field (Wilkes et al., 2023).

The array of products obtained thus far in a laboratory scale, span a wide range of applications, from repolymerization processes to pharmaceutical and material industries: (i) commodity chemicals valuable for diverse industrial applications, such as catechol, PG, and rhamnolipids; (ii) bioactive compounds utilized in pharmaceutical and cosmetic industries, such as PCA, GA, L-tyrosine, phenylalanine, glycolic acid, butyric acid, 4HB, and MLA; (iii) precursors utilized in polymer production, such as MA, PDC,  $\beta$ KA, DHB, and DAH; (iv) specialty chemicals abundantly used in food industry, such as VA, vanillin, and lycopene; (v) biodegradable and highly biocompatible biopolymers gaining momentum in the field of material science, such as BNC and PHAs; and (vi) others that are versatile enough to pervade diverse industrial fields, such as AA, CA, p-coumaric acid, SA, and BDO.

As the global plastic waste crisis intensifies, innovative and daring

strategies are deemed essential to effectively process and reintegrate plastics into the economy. Biological upcycling offers an alternative approach to managing plastic waste by converting it into valuable products, all the while minimizing humanity's dependence on finite fossil fuel resources. Nonetheless, several hurdles and challenges remain to be overcome. The efficiency and specificity of microbial upcycling processes need further optimization to enhance yield and product diversity. Additionally, scaling these biotechnological solutions to industrial levels requires addressing issues related to process stability and economic viability. Future research should focus on engineering robust microbial strains and optimizing metabolic pathways to improve the conversion rates of plastic monomers into desired products. Looking ahead, integrating these biological upcycling systems with existing waste management infrastructure could revolutionize recycling practices, making them more sustainable and eco-friendlier, while collaborative efforts between researchers, industry stakeholders, and policymakers will be crucial in driving the adoption and implementation of these technologies.

## Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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